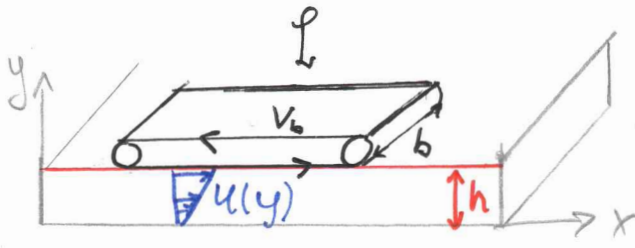


P1.1

1.1



known:

$v_b = 2.5 \text{ m/s}$

$L = 2 \text{ m}$

$b = 60 \text{ cm} = 0.6 \text{ m}$

$h = 3 \text{ cm} = 0.03 \text{ m}$

$\mu_{SAE30} = \left\{ \begin{array}{l} \text{Table A.3} \\ \text{F.S.P. 31} \end{array} \right\} = 0.29 \frac{\text{kg}}{\text{m}\cdot\text{s}}$

Assume: Negligible effects from air, linear flow profile, no slip

Find: $P(h, L, v_b, b, \mu)$, P in W

Solution: Use definition of shear stress & Force.

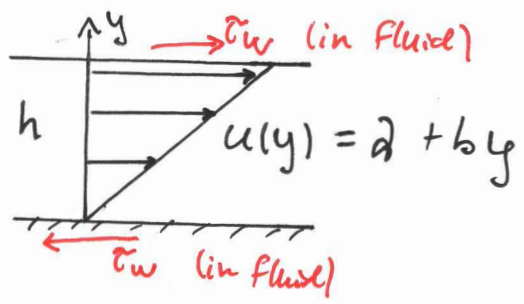
$F = \text{pressure} \times \text{area} = \tau_w \cdot A$

$E = \int F dl = F \cdot L$

$P = \frac{dE}{dt} = F \frac{L}{t} = F \cdot v_b$

$I = \tau_w \cdot A \cdot v_b \quad [A]$

Eq. (1.23) $\tau_w = \mu \frac{du}{dy} \quad [B]$



B.C: $u(y) = a + by$

$u(0) = 0 \Rightarrow a = 0$ (no slip)

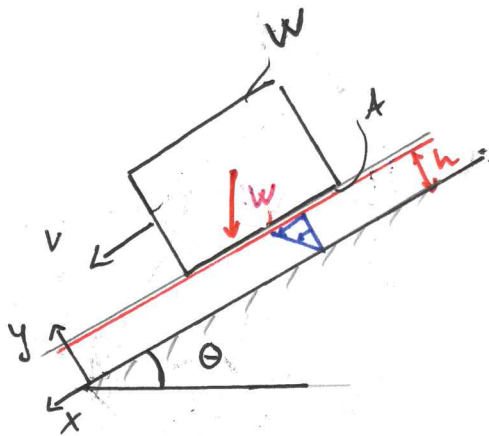
$u(h) = v_b \Rightarrow v_b = bh \Rightarrow b = \frac{v_b}{h}$

$\therefore u(y) = v_b \frac{y}{h}$ in [B]

$\tau_w = \mu \frac{d}{dy} \left(v_b \frac{y}{h} \right) = \frac{\mu v_b}{h}$ in [A]

$I(h, L, b, \mu, v_b) = \frac{\mu v_b}{h} \cdot A \cdot v_b = \left\{ A = b \cdot L \right\} = \mu \frac{v_b^2}{h} b \cdot L$

$I = 72.5 \text{ W}$



known:

$$m = 6 \text{ kg} \Rightarrow$$

$$\rightarrow F_g = 6 \cdot g = 58.86 \text{ N} = W$$

$$A = 35 \text{ cm}^2 = 0.0035 \text{ m}^2$$

$$\theta = 15^\circ$$

$$h = 1 \text{ mm} = 0.001 \text{ m}$$

$$\mu = \mu_{\text{STE30}} = \left\{ \text{Table A.3} \right\} = 0.29 \frac{\text{kg}}{\text{m}^2 \text{s}}$$

Linear flow profile

Assume: Negligible effects from air, no slip

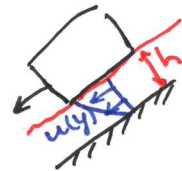
Derive: The terminal velocity V and calculate V .

Terminal velocity: $a_x = 0 \Rightarrow \sum F_x = 0$

Force equilibrium of the block:

$$\sum F_x = W \sin \theta - F_{\text{visc}} = 0 \quad [T]$$

$$F_{\text{visc}} = \tau_w \cdot A, \quad \tau_w = \mu \frac{du}{dy}, \quad \text{Eq (1.23)}$$



Linear flow profile $u(y) = a + by$

No slip: $u(0) = 0 = a$

$$u(h) = V = b \cdot h \Rightarrow b = \frac{V}{h} \Rightarrow u(y) = V \frac{y}{h}$$

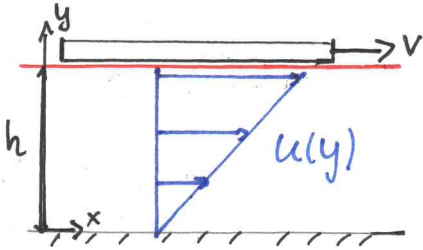
$$\tau_w = \mu \frac{du}{dy} \left(V \frac{y}{h} \right) = \mu \frac{V}{h} \Rightarrow F_{\text{visc}} = \mu \frac{V}{h} \cdot A \quad \text{in } [T]$$

$$W \sin \theta - \mu \frac{V}{h} \cdot A = 0 \Rightarrow$$

$$V = W \sin \theta \frac{h}{\mu A}$$

$$V = 15 \text{ m/s}$$

1.3



unknown:

$$V = 5.5 \text{ m/s}$$

$$h = 6 \text{ mm} = 0.006 \text{ m}$$

$$\mu = \left\{ \begin{array}{l} \text{Table A.3} \\ \text{F.S. 31} \end{array} \right\} = 1.49 \frac{\text{kg}}{\text{m}\cdot\text{s}}$$

$$\rho = \left\{ \text{Table A.3} \right\} = 1260 \frac{\text{kg}}{\text{m}^3}$$

Assume: Linear flow profile, no-slip $\begin{cases} u(0) = 0 \\ u(h) = V \end{cases}$

Find: a) Wall shear stress τ_w

b) Reynolds number (Re) if $L = h$

Solution: Use Eq. (1.23) to find τ_w

$$(1.23) \quad \tau_w = \mu \frac{du}{dy} \text{ ?}$$

$$u(y) = a + by$$

$$\text{B.C. } \left. \begin{array}{l} u(0) = 0 = a \\ u(h) = V = bh \end{array} \right\} u(y) = V \frac{y}{h} \Rightarrow \frac{du}{dy} = \frac{V}{h}$$

$$\tau_w = \mu \frac{V}{h} = 1365.83 \dots = 1366 \text{ Pa}$$

$$\text{b) } Re = \frac{\text{Inertia}}{\text{viscosity}} = \frac{\rho V L}{\mu} = \frac{\rho V h}{\mu} = 27.9 \dots = 28$$

Eq. (1.24)

21.4) Is the Stokes-Oseen formula dimensionally homogeneous?

1.4

$$F = \underbrace{3\pi}_{\text{I}} \underbrace{\mu DV}_{\text{II}} + \underbrace{\frac{9\pi}{16} \rho V^2 D^2}_{\text{III}}$$

Dimensions of units:

$$F: \frac{\text{kg} \cdot \text{m}}{\text{s}^2}$$

$$\mu: \frac{\text{kg}}{\text{m} \cdot \text{s}} \quad (\text{e.g. see Table A.3})$$

$$D: \text{m}$$

$$V: \frac{\text{m}}{\text{s}}$$

$$\rho: \frac{\text{kg}}{\text{m}^3} \quad (\text{e.g. see Table A.3})$$

$$\text{I: } \frac{F}{\text{kg} \cdot \text{m}} \cdot \frac{\text{s}^2}{\text{s}^2}$$

$$\text{II: } 3\pi \mu D V = \frac{\text{kg}}{\text{m} \cdot \text{s}} \cdot \text{m} \cdot \frac{\text{m}}{\text{s}} = \frac{\text{kg} \cdot \text{m}}{\text{s}^2} \quad \text{ok!}$$

$$\text{III: } \frac{9\pi}{16} \rho V^2 D^2 = \frac{\text{kg}}{\text{m}^3} \cdot \frac{\text{m}^2}{\text{s}^2} \cdot \text{m}^2 = \frac{\text{kg} \cdot \text{m}}{\text{s}^2} \quad \text{ok!}$$

The formula is dimensionally homogeneous!

P 1.13 1.5

$$\text{Known: } \eta_{\text{pump}} = \frac{Q \Delta P}{P} \quad \left| \quad \begin{array}{l} \Delta P = 35 \text{ lbf/in}^2 \quad (P = 16 \text{ hp}) \\ Q = 40 \text{ l/s} = 0,04 \frac{\text{m}^3}{\text{s}} \end{array} \right.$$

Task: Calculate the pump efficiency, η_{pump}

Solution: Convert all properties to SI units and calculate the efficiency.

Appendix C:

$$\Delta P = 35 \text{ lbf/in}^2 = 35 \cdot 6.8948 \text{ Pa} = 241318 \text{ Pa}$$

$$P = 16 \text{ hp} = 16 \cdot 745,7 \text{ W} = 11931,2 \text{ W}$$

Insert everything in the efficiency formula:

$$\eta_{\text{pump}} = \frac{0,04 \cdot 241318}{11931,2} = 0,81 \quad \text{or } 81\%$$

P1.25 1.6

Known: $T = 74^\circ \text{F}$

$$P = 14.5 \text{ lbf/in}^2$$

Air

Task: Estimate the fluid density of the air

Solution: Convert the temperature & pressure values into SI units and use the equation of state (ideal gas law)

Ideal gas law, Eq. (1.10)

$$P = \rho R T \Rightarrow \rho = \frac{P}{R T} \dots [A]$$

Appendix C:

$$P = 14.5 \text{ lbf/in}^2 = 14.5 \cdot 6.8948 \text{e}^3 \text{ Pa} = 99974.6 \text{ Pa}$$

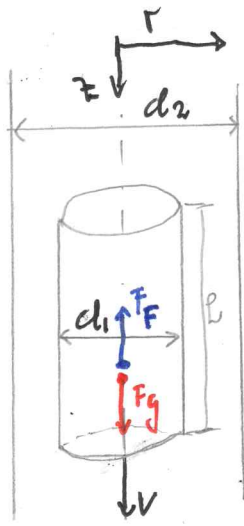
$$T = 74^\circ \text{F} = \frac{5}{9} (74^\circ \text{F} - 32)^\circ \text{C} = 23.3^\circ \text{C}, \quad T = 23.3^\circ \text{C} = 23.3 + 273 \text{ K} \\ = 296.3 \text{ K}$$

Appendix A:

Table A.2: $R_{\text{air}} = 287 \frac{\text{J}}{\text{kg K}}$

P in Pa, T in K and $R \rightarrow$ Eq [A] gives:

$$\rho = 1.18 \frac{\text{kg}}{\text{m}^3}$$



Known:

$$\begin{aligned}
 F_g &= 30 \text{ N} \\
 d_1 &= 0.06 \text{ m} \\
 L &= 0.4 \text{ m} \\
 d_2 &= 0.0604 \text{ m}
 \end{aligned}
 \left| \begin{array}{l}
 \text{SAE 50 oil:} \\
 \text{Table A.3} \rightarrow \\
 \mu = 0.86 \frac{\text{kg}}{\text{m}\cdot\text{s}}
 \end{array} \right.$$

Task: Find velocity, V , for the cylinder at zero acceleration (terminal velocity)

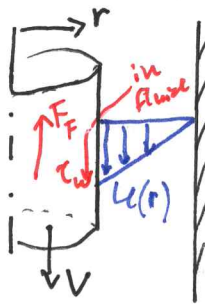
Assumes: Linear flow profile

Solution: Use force equilibrium for the cylinder and wall shear stress

$$\sum F = 0 = F_g - F_F \Rightarrow F_g = F_F \quad [A]$$

Definition of pressure/force: $F = \int \tau dA = \tau \cdot A = \tau L \pi d_1 \quad [B]$

Shear stress on cylinder:



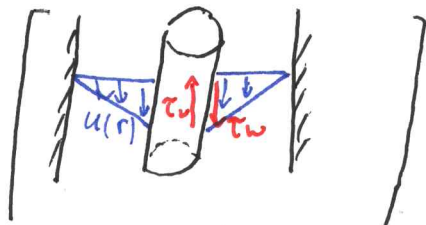
$$\tau_w = \mu \frac{du}{dr} \quad (1.23)$$

Linear flow profile gives: $u(r) = ar + b$

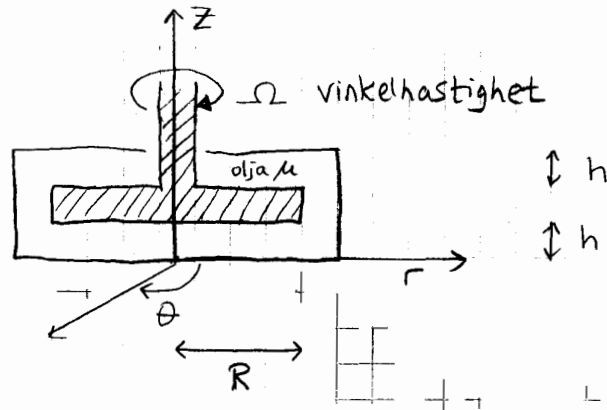
$$\left. \begin{aligned}
 \text{B.C: } u\left(\frac{d_2}{2}\right) &= 0 = a \frac{d_2}{2} + b \\
 u\left(\frac{d_1}{2}\right) &= V = a \frac{d_1}{2} + b
 \end{aligned} \right\} u(r) = \frac{2V}{d_1 - d_2} \cdot r - \frac{V d_2}{d_1 - d_2}$$

$\tau_w = \mu \frac{du}{dr} = \mu \frac{2V}{d_1 - d_2}$, The wall shear stress and F_F are [A] & [B] in opposite direction: $F_F = -\tau_w L \pi d_1 = F_g$

$$\Rightarrow F_g = -\mu \frac{2V}{d_1 - d_2} \cdot L \pi d_1 \Rightarrow V = \frac{-F_g (d_1 - d_2)}{L \pi d_1 2\mu} = 0.0925 \text{ m/s}$$



1,08

Givet:

Antag linjär hastighetsprofil och försumma skjuvspänningen vid skivändarna.

Sökt: Uttryck för vridmomentet på skivan M_{TOT}

Lösning: Vridmoment $M = F \cdot r$

I detta fall är kraften F , som krävs för att rotera skivan med en viss hastighet, samma kraft som krävs för att övervinna oljans motstånd till rörelse $F = \tau A$

$$M(r) = \tau(r, z=h) \cdot A \cdot r$$

$$\textcircled{1} M_{TOT} = \left(\int_0^{2\pi} \int_0^R \tau(r, z=h) \cdot r \cdot dA \right) \cdot 2$$

↙ för plattans under och översida

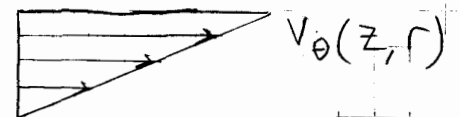
* Observera att, skjuvspänningen τ är en funktion av avståndet från plattans centrum, detta pga att den tangenta hastigheten $v_\theta = \Omega r$ ($\tau = \mu \frac{dv_\theta}{dz}$)

för varje punkt längs plattans radie gäller en annorlunda linjär hastighetsprofil

Nära plattans centrum



Långt ifrån plattans c



För linjär hastighetsprofil $\tau = \tau(r)$

$$v_\theta(r, z) = az + b$$

$$\text{Randvillkor } v_\theta(r, z=0) = 0$$

$$\left\{ \begin{array}{l} v_\theta(r, z=h) = \Omega r \end{array} \right.$$

$$v_\theta(r, z=0) = a \cdot 0 + b = 0 \Rightarrow b = 0$$

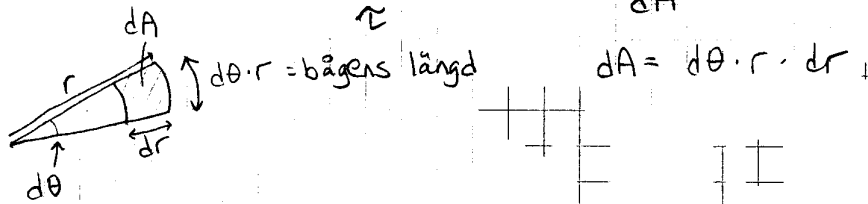
$$v_\theta(r, z=h) = a \cdot h = \Omega r \Rightarrow a = \frac{\Omega r}{h}$$

$$V_{\theta}(r, z) = \frac{\Omega r}{h} \cdot z$$

$$\tau = \mu \frac{dV_{\theta}(r, z)}{dz} = \mu \cdot \frac{\Omega r}{h}$$

① ger:

$$M_{\text{TOT}} = 2 \cdot \int_0^{2\pi} \int_0^R \underbrace{\mu \cdot \frac{\Omega r}{h}}_{\tau} \cdot r \cdot \underbrace{d\theta \cdot dr}_{dA}$$



$$M_{\text{TOT}} = 2 \cdot \int_0^{2\pi} \int_0^R \frac{\mu \Omega}{h} \cdot r^3 \cdot d\theta \cdot dr = 2 \cdot \frac{\mu \Omega}{h} \cdot 2\pi \cdot \frac{R^4}{4} = \frac{\mu \Omega \pi R^4}{h}$$

1.9

1.09

Givet: $u = B \frac{\Delta P}{\mu} (r_0^2 - r^2)$

↑ tryck
↑ viskositet
↑ radie

hastighet

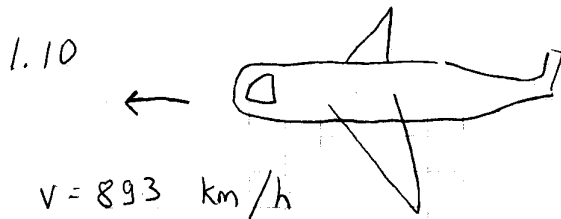
Sökt: Dimensionen på konstanten B

Lösning: $\left[\frac{m}{s} \right] = B \cdot \left[\frac{kg}{m \cdot s^2} \right] \left[\frac{m^2}{kg} \right] [m^2] = B \left[\frac{m^2}{s} \right]$

$$\Delta P = \frac{F}{A} = \frac{kg \cdot m}{m^2 \cdot s^2} = \left[\frac{kg}{m \cdot s^2} \right] \Rightarrow B = \left[\frac{1}{m} \right]$$

$$\mu = \left[\frac{kg}{m \cdot s} \right]$$

eller i de primära dimensionerna $B = \left[\frac{1}{L} \right]$



$$v = 893 \text{ km/h}$$

$$= \frac{893 \cdot 1000}{60 \cdot 60} = 248,1 \text{ m/s}$$

Sökt: Vid vilken höjd är planets mach-tal $M = 0,8$ då planets hastighet är $\bar{v} = 248,1 \text{ m/s}$?

Lösning - Machtalet ges av $M = \frac{v}{a}$ där $a =$ ljudets hastighet

Det finns 2 olika sätt att lösa problemet:

1. Ljudets hastighet $a = \frac{v}{M} = \frac{248,1}{0,8} = 310,1 \text{ m/s}$

Vid vilken höjd är ljudets hastighet $a = 310 \text{ m/s}$?

\Rightarrow Tabell [A.6] s. 773 $z = 7500 \text{ m}$

2. Ekv. [1.39] s. 37 $a = \sqrt{kRT}$ för ideal gas, där

tabell [A.4] torr luft \Rightarrow $\begin{cases} k = \frac{c_p}{c_v} = 1,4 \text{ specific-heat ratio} \\ R = 287 \frac{\text{m}^2}{\text{s}^2\text{K}} \\ T \text{ okänd} \end{cases}$

Lös ut T

$$M = \frac{v}{a} = \frac{v}{\sqrt{kRT}} \Rightarrow M^2 = \frac{v^2}{kRT} \Rightarrow kRTM^2 = v^2 \Rightarrow T = \frac{v^2}{kRM^2}$$

$$T = \frac{248,1^2}{1,4 \cdot 287 \cdot 0,8^2} = 239 \text{ K}$$

Tabell [A.6] \Rightarrow $z = 7500 \text{ m}$

1.11

Givet: Vatten som kokar vid 84°C

Sökt: Höjd över havet

Lösning: Tabell [A.5]

$x_0 = 80^{\circ}\text{C}$

$y_0 = 47,35 \text{ kPa}$

$x_1 = 90^{\circ}\text{C}$

$y_1 = 70,11 \text{ kPa}$

$$\text{interpolation } P_v(84^{\circ}\text{C}) = y = 47,35 + \frac{(70,11 - 47,35)(84 - 80)}{(90 - 80)}$$

$$= 47,35 + 9,104 = \underline{\underline{56,454 \text{ kPa}}}$$

(formel för interpolation)

$$y = y_0 + \frac{y_1 - y_0}{x_1 - x_0} (x - x_0)$$

Vid detta tryck kokar vatten vid 84°C . Vid vilken höjd över havet återfinns detta tryck? \Rightarrow Tabell A.6

Tabell [A.6]

$x_0 = 57718 \text{ Pa}$

$y_0 = 4500 \text{ m}$

$x_1 = 54008 \text{ Pa}$

$y_1 = 5000 \text{ m}$

$$\text{Interpolation för } z(56,454 \text{ kPa}) = y = 4500 + \frac{(5000 - 4500)(56,454 - 57,718)}{(54,008 - 57,718)}$$

$$= 4500 + 170,35 = \underline{\underline{4670,35 \text{ m}}}$$