

Fluid Mechanics - MTF053

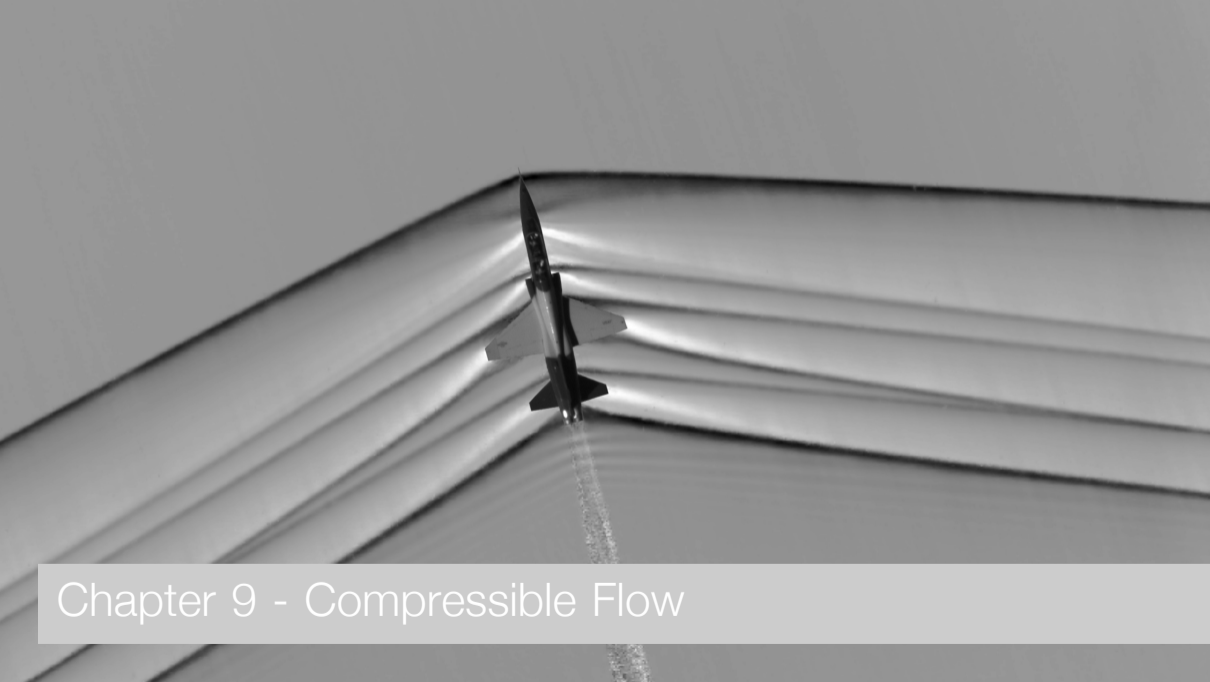
Lecture 18

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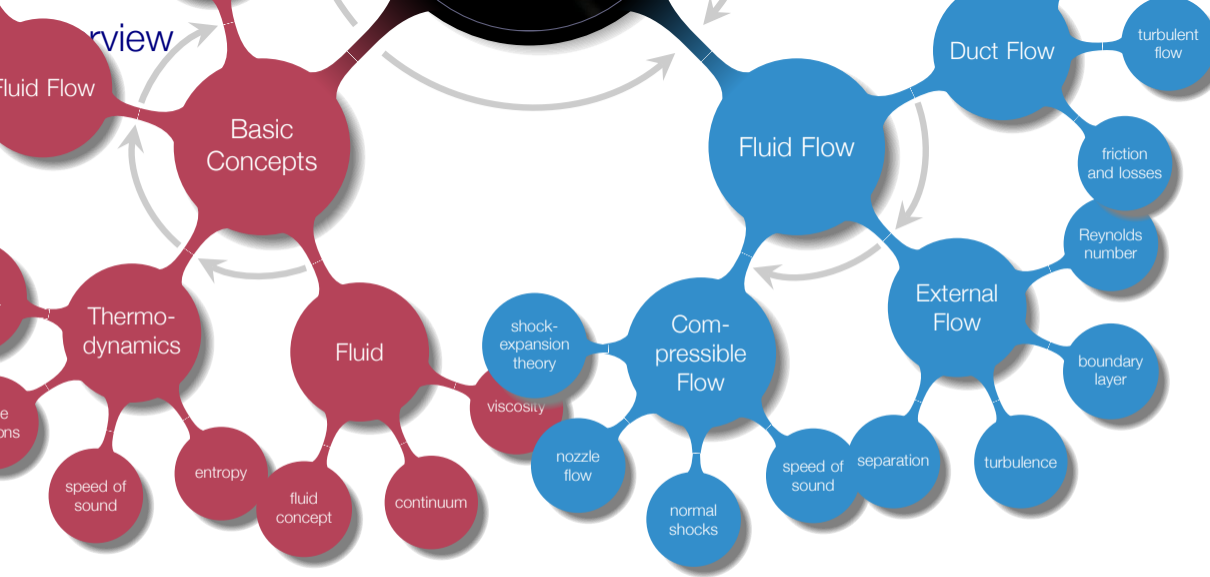
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Chapter 9 - Compressible Flow



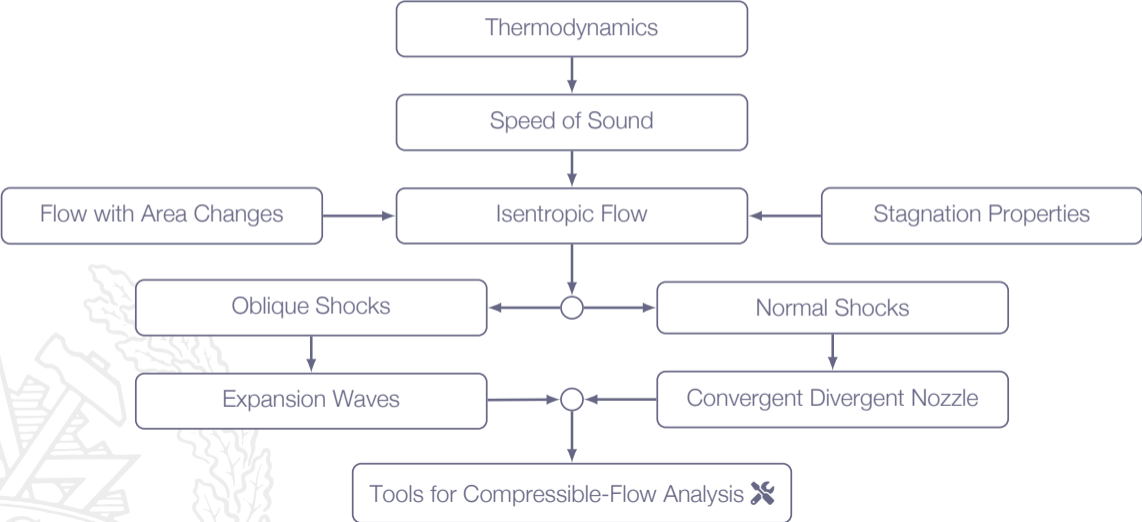
Learning Outcomes

- 4 Be **able to categorize** a flow and **have knowledge about** how to select applicable methods for the analysis of a specific flow based on category
- 37 **Understand and explain** basic concepts of compressible flows (the gas law, speed of sound, Mach number, isentropic flow with changing area, normal shocks, oblique shocks, Prandtl-Meyer expansion)

Let's go supersonic ...



Roadmap - Compressible Flow



Motivation

Compressible flow:

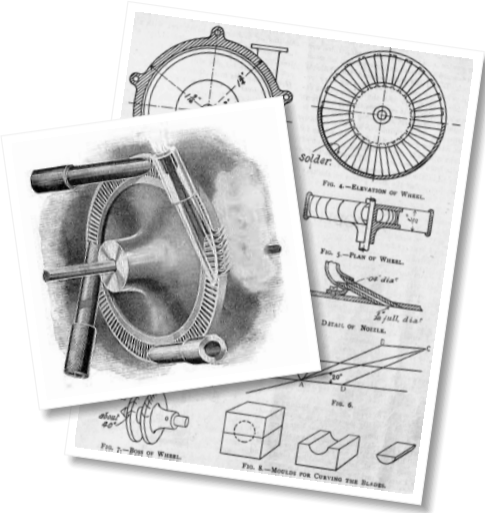
- ▶ flows where variations in density are significant
- ▶ most often high-speed gas flows (gas dynamics)
- ▶ fluids moving at speeds comparable to the speed of sound
- ▶ not common in liquids (would require very high pressures)



Historical Milestones



First supersonic flight - Charles Yeager 1947



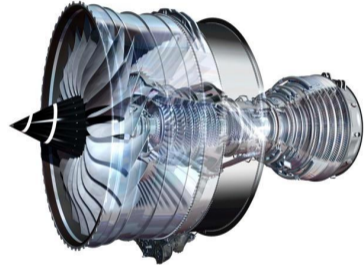
Steam turbine with convergent-divergent nozzles - Carl Gustav de Laval 1893



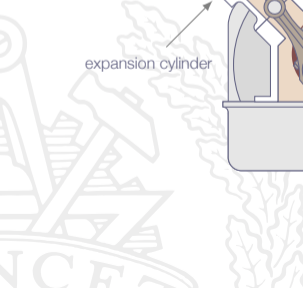
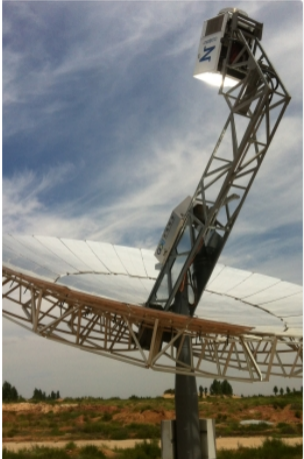
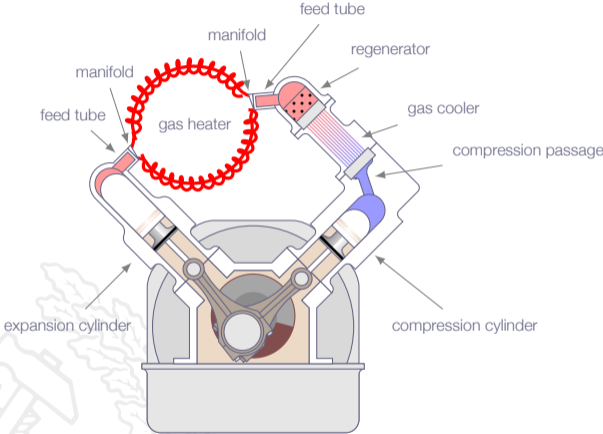
Compressible Flow Applications



Compressible Flow Applications



Compressible Flow Applications



Governing Equations

- ▶ With significant density changes follows substantial changes in pressure and temperature
- ▶ The energy equation must be included
- ▶ Four equations:
 1. Continuity
 2. Momentum
 3. Energy
 4. Equation of state
- ▶ Unknowns: ρ , p , T , and \mathbf{V}
- ▶ The four equations must be solved simultaneously

Mach Number Regimes

Incompressible flow

- ▶ insignificant density changes

Subsonic flow

- ▶ local and global Mach number less than unity

Transonic flow

- ▶ subsonic flow with regions of supersonic flow (local Mach number can be higher than one)
- ▶ supersonic flow with regions of subsonic flow (local Mach number can be less than one)

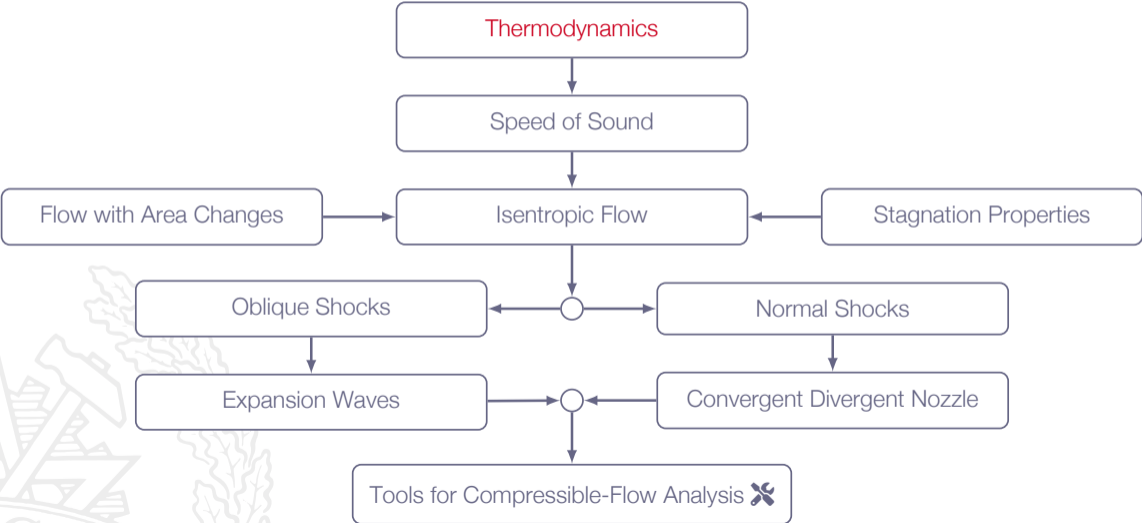
Supersonic flow

- ▶ local and global Mach number higher than one

Hypersonic flow

- ▶ Mach number higher than 5.0

Roadmap - Compressible Flow



Ratio of Specific Heats

- ▶ The ratio of specific heats is important in compressible flow

$$\gamma = \frac{C_p}{C_v}$$

- ▶ γ is a fluid property
- ▶ For moderate temperatures γ is a constant
- ▶ For higher temperatures γ varies with temperature
- ▶ For air, $\gamma = 1.4$

Equation of State

In the following, we will assume that the ideal gas law is applicable and that the specific heats are constants:

$$p = \rho RT$$

$$R = C_p - C_v = \text{const}$$

$$\gamma = \frac{C_p}{C_v} = \text{const}$$

Auxiliary relations:

$$C_v = \frac{R}{\gamma - 1}, C_p = \frac{\gamma R}{\gamma - 1}$$

Internal Energy and Enthalpy

Constant specific heats:

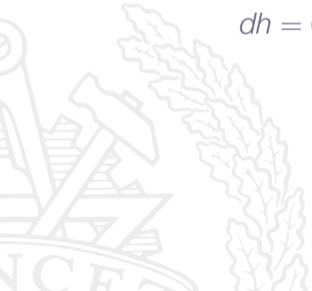
$$d\hat{u} = C_v dT$$

$$dh = C_p dT$$

Variable specific heats:

$$\hat{u} = \int C_v dT$$

$$h = \int C_p dT$$



Isentropic Relations

First law of thermodynamics

$$\delta q + \delta w = de$$

For reversible processes: $\delta w = -pdv$ (where $v = p/\rho$)

$$h = e + \frac{p}{\rho} = e + pv \Rightarrow dh = de + pdv + vdp$$

$$\delta q = dh - vdp$$

Second law of thermodynamics

$$ds = \frac{\delta q_{rev}}{T} = \frac{\delta q}{T} + ds_{irev} \Rightarrow ds \geq \frac{\delta q}{T}$$

Isentropic Relations

compute entropy change from the first and second law of thermodynamics
(assuming reversible heat addition)

$$Tds = dh - \frac{dp}{\rho}$$

for perfect gases, $dh = C_p dT$

$$\int_1^2 ds = \int_1^2 C_p \frac{dT}{T} - R \int_1^2 \frac{dp}{\rho}$$

for constant specific heats (calorically perfect)

$$s_2 - s_1 = C_p \ln \frac{T_2}{T_1} - R \ln \frac{\rho_2}{\rho_1} = C_v \ln \frac{T_2}{T_1} - R \ln \frac{\rho_2}{\rho_1}$$

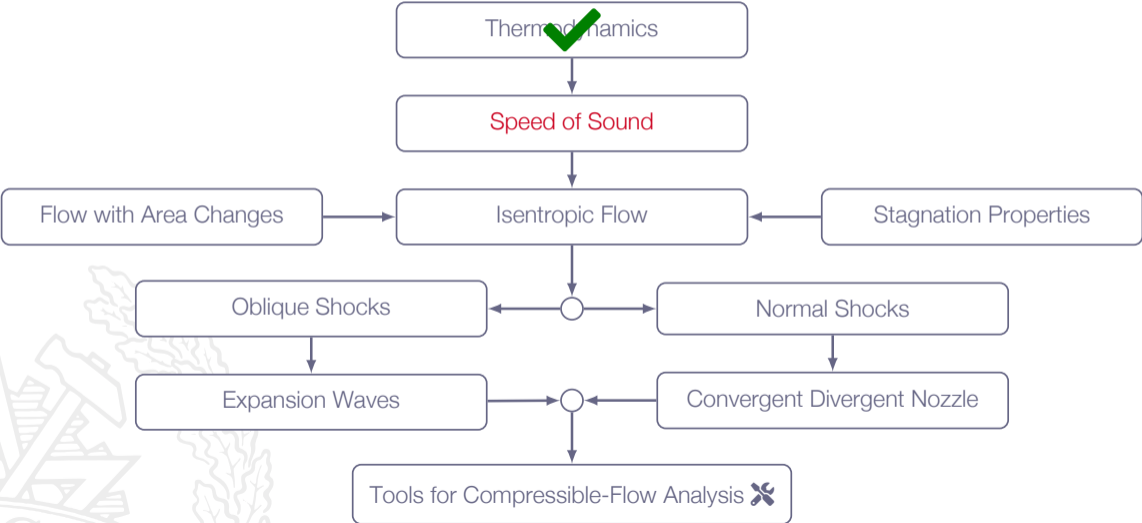
Isentropic Relations

$$s_2 - s_1 = C_p \ln \frac{T_2}{T_1} - R \ln \frac{\rho_2}{\rho_1} = C_v \ln \frac{T_2}{T_1} - R \ln \frac{\rho_2}{\rho_1}$$

for isentropic flow ($s_2 = s_1$) we get

$$\frac{\rho_2}{\rho_1} = \left(\frac{T_2}{T_1} \right)^{\gamma/(\gamma-1)} = \left(\frac{\rho_2}{\rho_1} \right)^{\gamma}$$

Roadmap - Compressible Flow

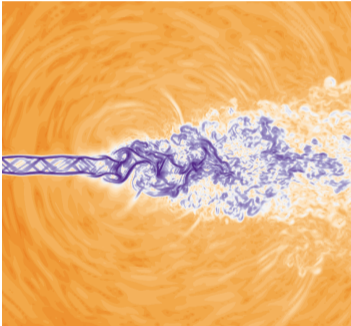
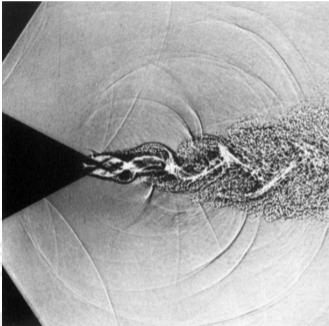


Speed of Sound

- ▶ The rate of propagation of a pressure pulse of infinitesimal strength through a fluid at rest
- ▶ Related to the molecular activity of the fluid
- ▶ A thermodynamic property



Speed of Sound



Speed of Sound

frame of reference fixed to fluid

$$\begin{array}{c} \rho \\ \rho \\ T \\ V = 0 \end{array} \quad \begin{array}{c} \xleftarrow{C} \\ \parallel \\ \rho + \Delta\rho \\ \rho + \Delta\rho \\ T + \Delta T \\ V = \Delta V \\ \xleftarrow{\quad} \end{array}$$

frame of reference following the wave

$$\begin{array}{c} \rho \\ \rho \\ T \\ V = C \\ \xrightarrow{\quad} \end{array} \quad \begin{array}{c} \parallel \\ \rho + \Delta\rho \\ \rho + \Delta\rho \\ T + \Delta T \\ V = C - \Delta V \\ \xrightarrow{\quad} \end{array}$$

Speed of Sound

frame of reference following the wave

continuity:

$$\begin{array}{ccc} \rho & & \rho + \Delta\rho \\ p & & p + \Delta p \\ T & & T + \Delta T \\ \hline V = C & & V = C - \Delta V \end{array}$$

$$\rho AC = (\rho + \Delta\rho)A(C - \Delta V)$$

$$\Delta V = C \frac{\Delta\rho}{\rho + \Delta\rho}$$

Note! there are no gradients in the flow so viscous effects are confined to the interior of the wave

Speed of Sound

frame of reference following the wave

momentum:

$$\begin{array}{ccc} \rho & & \rho + \Delta\rho \\ p & & p + \Delta p \\ T & & T + \Delta T \\ v = c & & v = c - \Delta v \end{array}$$

$$pA - (p + \Delta p)A = (\rho AC)(C - \Delta V - C) \Rightarrow \Delta p = \rho C \Delta V$$

with ΔV from the continuity equation we get

$$C^2 = \frac{\Delta p}{\Delta \rho} \left(1 + \frac{\Delta \rho}{\rho} \right)$$

Note! the larger $\Delta \rho / \rho$, the higher the propagation velocity

Speed of Sound

In the limit of infinitesimal strength $\Delta\rho \rightarrow 0$ and thus

$$C^2 = a^2 = \frac{\partial p}{\partial \rho}$$

- ▶ There is no added heat and thus the process adiabatic
- ▶ For weak waves the process can also be assumed to be reversible

$$a^2 = \left. \frac{\partial p}{\partial \rho} \right|_s$$



Speed of Sound

$$a^2 = \left. \frac{\partial p}{\partial \rho} \right|_s$$

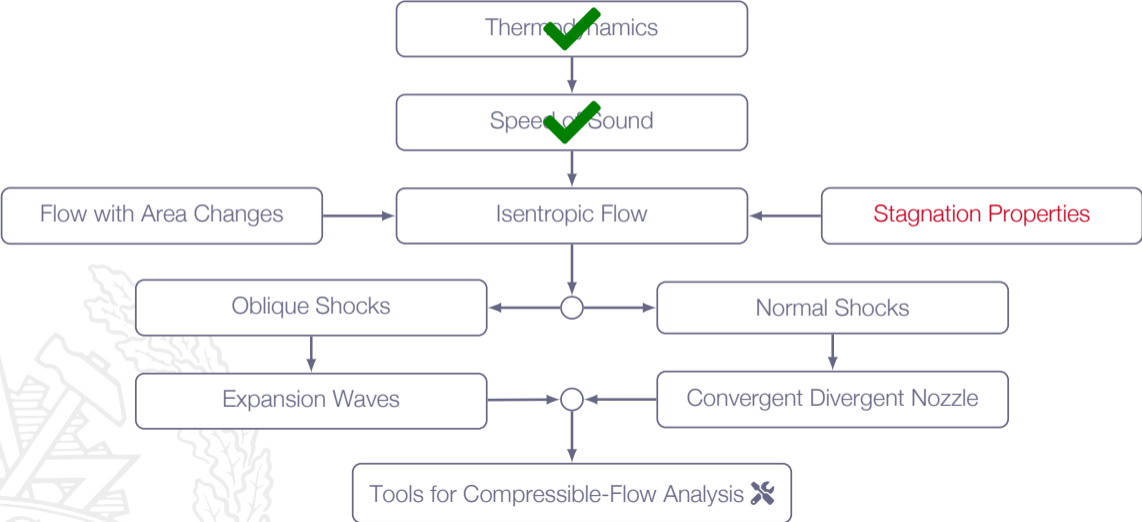
The isentropic relation gives

$$p = \rho^\gamma \Rightarrow \frac{\partial p}{\partial \rho} = \gamma \rho^{\gamma-1} = \gamma \frac{p}{\rho} = \gamma RT$$

and thus

$$a = \sqrt{\gamma RT}$$

Roadmap - Compressible Flow



Stagnation Enthalpy

Consider high-speed gas flow past an insulated wall

$$h_1 + \frac{1}{2}V_1^2 + gz_1 = h_2 + \frac{1}{2}V_2^2 + gz_2 - q + w_\nu$$

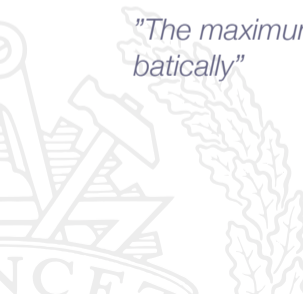
- ▶ differences in potential energy extremely small
- ▶ outside of the boundary layer, heat transfer and viscous work are zero

$$h_1 + \frac{1}{2}V_1^2 = h_2 + \frac{1}{2}V_2^2 = \text{const}$$

Stagnation Enthalpy

$$h + \frac{1}{2}V^2 = h_o$$

"The maximum enthalpy that the fluid would achieve if brought to rest adiabatically"



Stagnation Temperature

For a calorically perfect gas $h = C_p T$

$$h + \frac{1}{2}V^2 = h_o$$

$$C_p T + \frac{1}{2}V^2 = C_p T_o$$

Where T_o is the stagnation temperature



Mach Number Relations

$$C_p T + \frac{1}{2} V^2 = C_p T_o \Rightarrow 1 + \frac{V^2}{2C_p T} = \frac{T_o}{T}$$

$$C_p T = \frac{\gamma R}{\gamma - 1} T = \frac{\gamma R T}{\gamma - 1} = \frac{a^2}{\gamma - 1}$$

$$\frac{T_o}{T} = 1 + \left(\frac{\gamma - 1}{2} \right) M^2$$

Mach Number Relations

Since $a \propto T^{1/2}$ we get

$$\frac{a_0}{a} = \left(\frac{T_0}{T} \right)^{1/2} = \left[1 + \left(\frac{\gamma - 1}{2} \right) M^2 \right]^{1/2}$$



Mach Number Relations

If the flow is adiabatic and reversible (isentropic), we may use the isentropic relations

$$\frac{\rho_o}{\rho} = \left(\frac{T_o}{T}\right)^{\gamma/(\gamma-1)} = \left[1 + \left(\frac{\gamma-1}{2}\right)M^2\right]^{\gamma/(\gamma-1)}$$

$$\frac{\rho_o}{\rho} = \left(\frac{T_o}{T}\right)^{1/(\gamma-1)} = \left[1 + \left(\frac{\gamma-1}{2}\right)M^2\right]^{1/(\gamma-1)}$$



Stagnation Properties

- ▶ p_o and ρ_o - the pressure and density that the flow would achieve if brought to rest isentropically
- ▶ All stagnation properties are constants in an isentropic flow
- ▶ h_o , T_o , and a_o are constants in an adiabatic flow but not necessarily p_o and ρ_o
- ▶ p_o and ρ_o will vary throughout an adiabatic flow as the entropy changes due to friction or shocks

Critical Properties

Another useful set of reference variables is the critical properties (sonic conditions)

$$\frac{T_o}{T} = 1 + \left(\frac{\gamma - 1}{2}\right) M^2 = \{M = 1.0\} = 1 + \left(\frac{\gamma - 1}{2}\right) = \left(\frac{2 + \gamma - 1}{2}\right) = \left(\frac{\gamma + 1}{2}\right)$$



Critical Properties

$$\frac{T^*}{T_o} = \left(\frac{2}{\gamma + 1} \right)$$

$$\frac{a^*}{a_o} = \left(\frac{2}{\gamma + 1} \right)^{1/2}$$

$$\frac{p^*}{p_o} = \left(\frac{2}{\gamma + 1} \right)^{\gamma/(\gamma-1)}$$

$$\frac{\rho^*}{\rho_o} = \left(\frac{2}{\gamma + 1} \right)^{1/(\gamma-1)}$$

Critical Properties

Air $\gamma = 1.4$

$$\frac{T^*}{T_o} = \left(\frac{2}{\gamma + 1} \right) = 0.8333$$

$$\frac{a^*}{a_o} = \left(\frac{2}{\gamma + 1} \right)^{1/2} = 0.9129$$

$$\frac{p^*}{p_o} = \left(\frac{2}{\gamma + 1} \right)^{\gamma/(\gamma-1)} = 0.5283$$

$$\frac{\rho^*}{\rho_o} = \left(\frac{2}{\gamma + 1} \right)^{1/(\gamma-1)} = 0.6339$$