# Fluid Mechanics - MTF053 Lecture 14

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#### Chapter 7 - Flow Past Immersed Bodies



# Learning Outcomes

- 4 Be **able to categorize** a flow and **have knowledge about** how to select applicable methods for the analysis of a specific flow based on category
- 6 Explain what a boundary layer is and when/where/why it appears
- 21 **Explain** how the flat plate boundary layer is developed (transition from laminar to turbulent flow)
- 22 Explain and use the Blasius equation
- 23 Define the Reynolds number for a flat plate boundary layer
- 24 Explain what is characteristic for a turbulent flow
- 29 Explain flow separation (separated cylinder flow)
- 30 **Explain** how to delay or avoid separation
- 31 Derive the boundary layer formulation of the Navier-Stokes equations
- 32 Understand and explain displacement thickness and momentum thickness
- 33 **Understand**, **explain** and **use** the concepts drag, friction drag, pressure drag, and lift

Let's take a deep dive into boundary-layer theory

## Roadmap - Flow Past Immersed Bodies



These lecture notes covers chapter 7 in the course book and additional course material that you can find in the following documents

MTF053\_Equation-for-Boundary-Layer-Flows.pdf

MTF053\_Turbulence.pdf

Address of the second s

"Understanding the mechanisms behind flow-related forces is a key factor to success in many engineering applications"

S. MB 7177

Significant viscous effects near the surface of an immersed body

Nearly inviscid far from the body

Unconfined - boundary layers are free to grow

Most often CFD or experiments are needed to analyze an external flow unless the geometry is very simple

## Roadmap - Flow Past Immersed Bodies



## **Reynolds Number Effects**



## **Reynolds Number Effects**



Note! ReL and the local Reynolds number Rex are not the same

### Roadmap - Flow Past Immersed Bodies



We will derive a set of equations suitable for **boundary-layer flow analysis** 

Starting point: the **non-dimensional equations** derived in Chapter 5

We will assume two-dimensional, incompressible, steady-state flow

We will do an **order-of-magnitude** comparison of all the terms in the governing equations on non-dimensional form and identify terms that can be neglected in a **thin-boundary-layer** flow

#### continuity:

$$\frac{\partial u^*}{\partial x^*} + \frac{\partial v^*}{\partial y^*} = 0$$

x-momentum:  $u^* \frac{\partial u^*}{\partial x^*} + v^* \frac{\partial u^*}{\partial y^*} = -\frac{\partial p^*}{\partial x^*} + \frac{1}{Re_L} \left( \frac{\partial^2 u^*}{\partial x^{*2}} + \frac{\partial^2 u^*}{\partial y^{*2}} \right)$ y-momentum:  $u^* \frac{\partial v^*}{\partial x^*} + v^* \frac{\partial v^*}{\partial y^*} = -\frac{\partial p^*}{\partial y^*} + \frac{1}{Re_L} \left( \frac{\partial^2 v^*}{\partial x^{*2}} + \frac{\partial^2 v^*}{\partial y^{*2}} \right)$ 



To be able to find the relative sizes of different terms in the equations, we will first have a look at the flow parameters and operators

$$u^* = u/U_{\infty} \sim 1$$

 $x^* = x/L \sim 1$ 

$$y^* = y/L \sim \delta^*$$

 $\delta$  denotes boundary layer thickness and  $\delta^* = \delta/L$ 

**Note!** here,  $u^*$  is **not** the friction velocity and  $\delta^*$  is **not** the displacement thickness

What about derivatives?

$$\frac{\partial u^*}{\partial y^*} \sim \frac{1-0}{\delta^*} = \frac{1}{\delta^*}$$



 $y^* \to 0 \Rightarrow u^* \to 0$ 

 $v^* \to \delta^* \Rightarrow u^* \to 1$ 

What about derivatives?

$$\frac{\partial u^*}{\partial y^*} \sim \frac{1-0}{\delta^*} = \frac{1}{\delta^*}$$



$$y^* \to 0 \Rightarrow u^* \to 0, \ \frac{\partial u^*}{\partial y^*} \to \frac{1}{\delta^*}$$

$$\frac{\partial^2 u^*}{\partial y^{*2}} = \frac{\partial}{\partial y^*} \frac{\partial u^*}{\partial y^*} \sim \frac{|0 - 1/\delta^*|}{\delta^*} = \frac{1}{\delta^{*2}}$$



$$\frac{\partial u^*}{\partial x^*} \sim \frac{|0-1|}{1-0} = 1$$



continuity:

$$\frac{\partial u^*}{\partial x^*}_{\sim \frac{1}{1}} + \underbrace{\frac{\partial v^*}{\partial y^*}}_{\sim \frac{?}{\delta^*}} = 0 \Rightarrow v^* \sim \delta^*$$

 $\frac{\partial v^*}{\partial y^*}$  must be of the same order of magnitude as  $\frac{\partial u^*}{\partial x^*}$  in order to fulfill the continuity equation





 $y^* \to 0 \Rightarrow v^* \to 0$ 

$$\frac{\partial \mathbf{v}^*}{\partial \mathbf{y}^*} \sim \frac{\delta^*}{\delta^*} = 1$$

$$\frac{\partial v^*}{\partial y^*} \sim \frac{\delta^*}{\delta^*} = 1$$
$$\frac{\partial^2 v^*}{\partial y^{*2}} = \frac{\partial}{\partial y^*} \frac{\partial v^*}{\partial y^*} \sim \frac{|0-1|}{\delta^*} = \frac{1}{\delta^*}$$



$$y^* \to 0 \Rightarrow v^* \to 0, \ \frac{\partial v^*}{\partial y^*} \to 1$$



$$\frac{\partial v^*}{\partial x^*} \sim \frac{|0 - \delta^*|}{1 - 0} = \delta^*$$



x-momentum:

$$\underbrace{u^* \frac{\partial u^*}{\partial x^*}}_{\sim 1 \times 1 = 1} + \underbrace{v^* \frac{\partial u^*}{\partial y^*}}_{\sim \delta^* \frac{1}{\delta^*} = 1} = -\frac{\partial p^*}{\partial x^*} + \frac{1}{Re_L} \left( \underbrace{\frac{\partial^2 u^*}{\partial x^{*2}}}_{\sim 1} + \underbrace{\frac{\partial^2 u^*}{\partial y^{*2}}}_{\sim \frac{1}{\delta^*}} \right)$$

the boundary layer is assumed to be very thin  $\Rightarrow \delta^* \ll 1$  and thus

$$\frac{\partial^2 u^*}{\partial x^{*2}} \ll \frac{\partial^2 u^*}{\partial y^{*2}}$$

assuming the inertial forces to be of the same size as the friction forces in the boundary layer we get:  $1/Re_L \sim {\delta^*}^2$ 

y-momentum:

$$\underbrace{U^* \frac{\partial v^*}{\partial x^*}}_{\sim 1 \times \delta^* = \delta^*} + \underbrace{v^* \frac{\partial v^*}{\partial y^*}}_{\sim \delta^* \frac{\delta^*}{\delta^*} = \delta^*} = -\frac{\partial \rho^*}{\partial y^*} + \underbrace{\frac{1}{\operatorname{Re}_L}}_{\sim \delta^{*2}} \left( \underbrace{\frac{\partial^2 v^*}{\partial x^{*2}}}_{\sim \delta^*} + \underbrace{\frac{\partial^2 v^*}{\partial y^{*2}}}_{\sim \frac{1}{\delta^*}} \right)$$

examining the equation we see that all terms are at most of size  $\delta^* \Rightarrow \frac{\partial \rho^*}{\partial v^*} \sim \delta^*$ 

 $\delta^*$  is small  $\Rightarrow p$  is independent of y

The pressure can be assumed to be constant in the vertical direction through the boundary layer and thus p = p(x)



$$|\boldsymbol{\rho}^*_{\delta} - \boldsymbol{\rho}^*_{W}| \approx \frac{\partial \boldsymbol{\rho}^*}{\partial y^*} \delta^* \sim {\delta^*}^2$$

With the knowledge gained, we now move back to the dimensional equations

laminar

#### turbulent

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$
$$u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} = -\frac{1}{\rho}\frac{d\rho}{dx} + v\frac{\partial^2 u}{\partial y^2}$$

$$\begin{aligned} \frac{\partial \overline{u}}{\partial x} &+ \frac{\partial \overline{v}}{\partial y} = 0\\ \overline{u}\frac{\partial \overline{u}}{\partial x} &+ \overline{v}\frac{\partial \overline{u}}{\partial y} = -\frac{1}{\rho}\frac{d\overline{\rho}}{dx} + \nu\frac{\partial^2 \overline{u}}{\partial y^2} - \frac{\partial}{\partial y}\overline{u'v'} \end{aligned}$$



#### Limitations

- . The boundary layer equations do not apply close to the start of the boundary layer where  $\frac{\partial u^*}{\partial x^*} \gg 1$
- 2. The equations are derived assuming a thin boundary layer

The pressure derivative can be replaced with a velocity derivative

Outside of the boundary layer the flow is inviscid  $\Rightarrow$  we can use the Bernoulli equation

$$p + \frac{1}{2}\rho U_{\infty}^{2} = const \Rightarrow \frac{dp}{dx} + \rho U_{\infty} \frac{dU_{\infty}}{dx} = 0 \Rightarrow -\frac{1}{\rho} \frac{dp}{dx} = U_{\infty} \frac{dU}{dx}$$

#### laminar boundary layer

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$
$$u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} = U_{\infty}\frac{dU_{\infty}}{dx} + v\frac{\partial^2 u}{\partial y^2}$$

Two equations and two unknowns  $\Rightarrow$  possible to solve  $\bigcirc$ 

**Note!** the boundary layer equations can be used for curved surfaces if the boundary layer thickness  $\delta$  is small compared to the curvature radius *r* 

