

Fluid Mechanics - MTF053

Lecture 2

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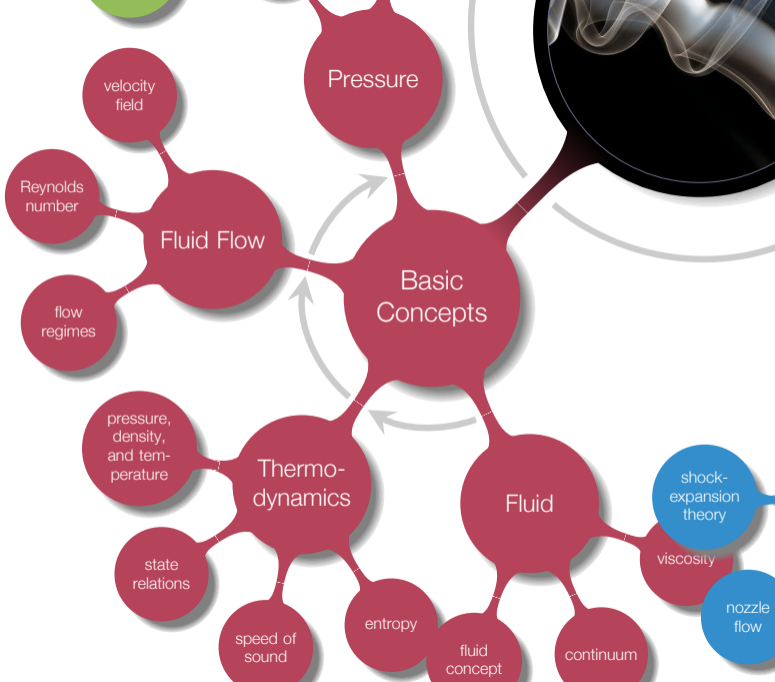




Chapter 1 - Introduction



Overview

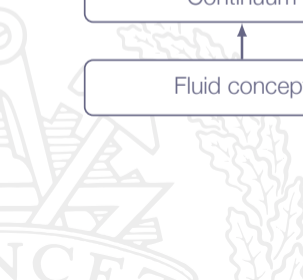
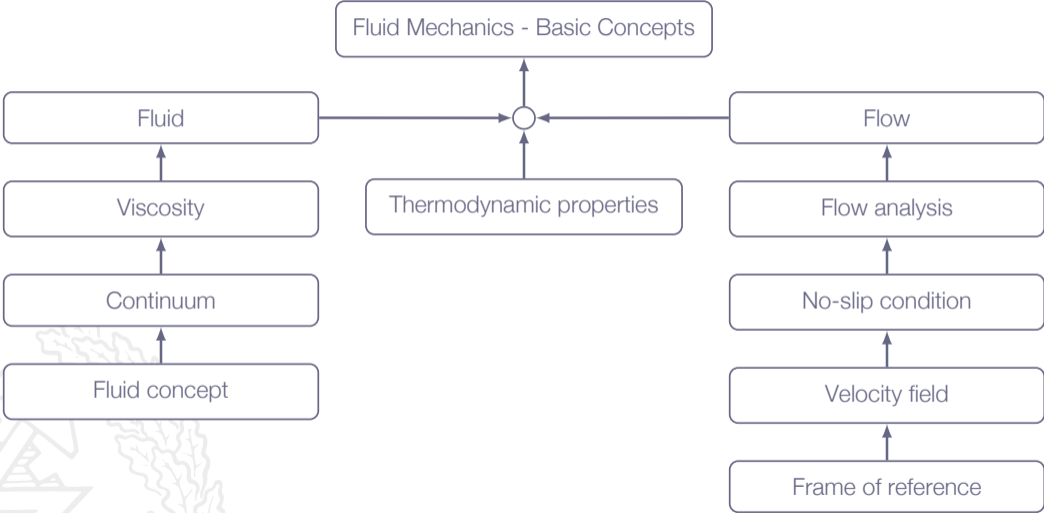


Learning Outcomes

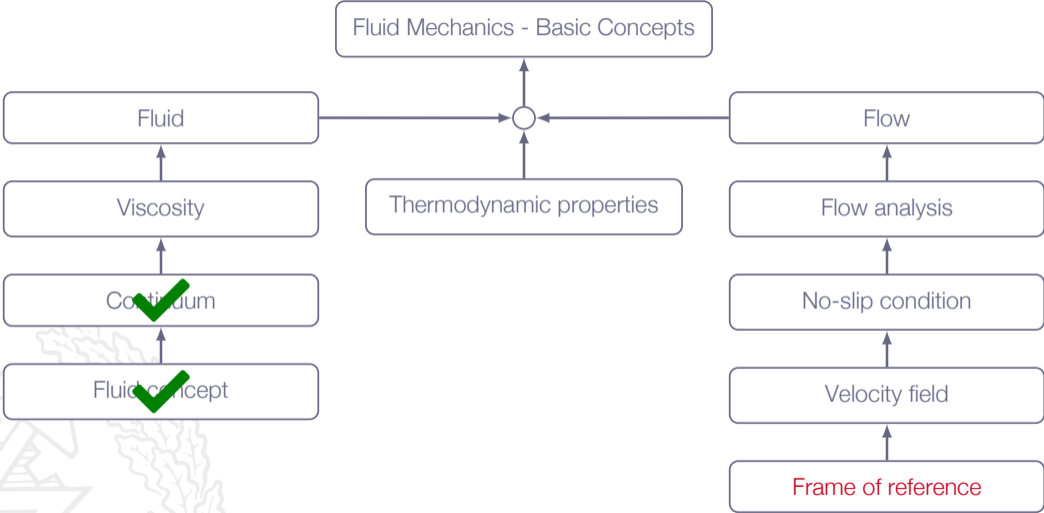
- 1 **Explain** the difference between a fluid and a solid in terms of forces and deformation
- 2 **Understand** and be able to explain the viscosity concept
- 3 **Define** the Reynolds number
- 5 **Explain** the difference between Lagrangian and Eulerian frame of reference and know when to use which approach
- 7 **Explain** the concepts: streamline, pathline and streakline
- 8 **Understand** and be able to **explain** the concept shear stress
- 9 **Explain** how to do a force balance for fluid element (forces and pressure gradients)
- 10 **Understand and explain** buoyancy and cavitation
- 16 **Understand** and **explain** the concept Newtonian fluid

in this lecture we will find out what a fluid flow is

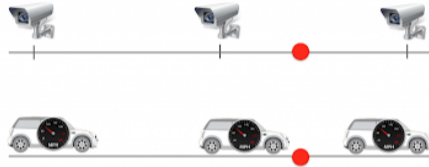
Roadmap - Introduction to Fluid Mechanics



Roadmap - Introduction to Fluid Mechanics



Frame of Reference



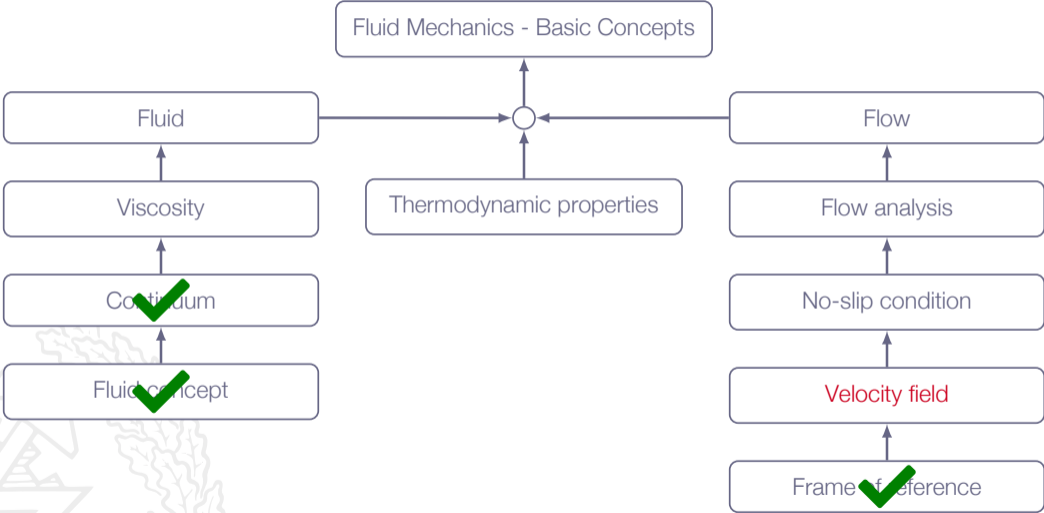
- ▶ Eulerian

- ▶ fluid properties as function of position and time
- ▶ most often used in fluid mechanics

- ▶ Lagrangian

- ▶ follows a system in time and space
- ▶ can be used in fluid mechanics
- ▶ most often used in solid mechanics

Roadmap - Introduction to Fluid Mechanics



Properties of the Velocity Field

- ▶ The fluid velocity is a function of position and time
- ▶ Three components u , v , and w (one in each spatial direction)

$$\mathbf{V}(x, y, z, t) = u(x, y, z, t)\mathbf{e}_x + v(x, y, z, t)\mathbf{e}_y + w(x, y, z, t)\mathbf{e}_z$$



Properties of the Velocity Field

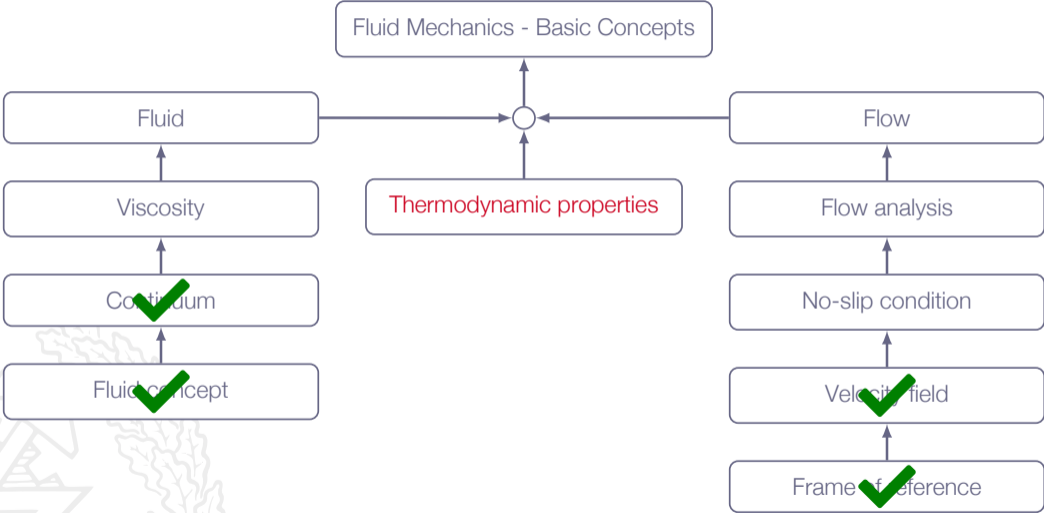
Acceleration:

$$\mathbf{V}(x, y, z, t) = u(x, y, z, t)\mathbf{e}_x + v(x, y, z, t)\mathbf{e}_y + w(x, y, z, t)\mathbf{e}_z$$

$$\mathbf{a} = \frac{d\mathbf{V}}{dt} = \frac{\partial\mathbf{V}}{\partial t} + \left(\frac{\partial\mathbf{V}}{\partial x}\right) \left(\frac{\partial x}{\partial t}\right) + \left(\frac{\partial\mathbf{V}}{\partial y}\right) \left(\frac{\partial y}{\partial t}\right) + \left(\frac{\partial\mathbf{V}}{\partial z}\right) \left(\frac{\partial z}{\partial t}\right)$$

$$\frac{d\mathbf{V}}{dt} = \frac{\partial\mathbf{V}}{\partial t} + u\frac{\partial\mathbf{V}}{\partial x} + v\frac{\partial\mathbf{V}}{\partial y} + w\frac{\partial\mathbf{V}}{\partial z}$$

Roadmap - Introduction to Fluid Mechanics



Thermodynamic Properties

- ▶ Thermodynamic properties describe the state of a system, i.e., a collection of matter of fixed identity which interacts with its surroundings
- ▶ In this course, the system will be a small fluid element, and all properties will be assumed to be continuum properties of the flow field



Thermodynamic Properties

- ▶ Pressure p Pa
- ▶ Density ρ kg/m³
- ▶ Temperature T K

most common properties



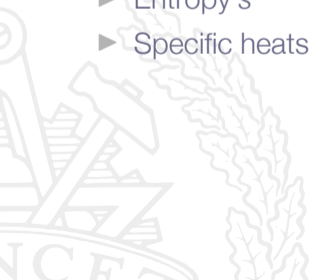
Thermodynamic Properties

- ▶ Pressure p Pa
- ▶ Density ρ kg/m³
- ▶ Temperature T K

- ▶ Internal energy \hat{u}
- ▶ Enthalpy $h = \hat{u} + p/\rho$
- ▶ Entropy s
- ▶ Specific heats C_p and C_v

most common properties

work, heat, and energy balances



Thermodynamic Properties

- ▶ Pressure p Pa
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- ▶ Entropy s
- ▶ Specific heats C_p and C_v

- ▶ Viscosity μ
- ▶ Thermal conductivity k

most common properties

work, heat, and energy balances

friction and heat conduction

Thermodynamic Properties

- ▶ For a single-phase substance, two basic properties are sufficient to get the values of all others

$$\rho = \rho(p, T), h = h(p, T), \mu = \mu(p, T)$$

- ▶ In the following it will be assumed that all thermodynamic properties exists as point functions in a flowing fluid
 - ▶ large enough number of molecules
 - ▶ any changes are slower than the flow time scale \Rightarrow equilibrium

Thermodynamic Properties

Pressure: p [Pa]

- ▶ the compression stress at a point in a static fluid
- ▶ a fluid flow is often driven by pressure gradients
- ▶ if the pressure drops below the vapor pressure in a liquid, vapor bubbles will form

Temperature: T [K]

- ▶ related to internal energy
- ▶ large temperature differences \Rightarrow heat transfer may be important

Density: ρ [kg/m³]

- ▶ mass per unit volume
- ▶ nearly constant in liquids (incompressible) - for water, the density increases about one percent for a pressure increase by a factor of 220
- ▶ not constant for gases

$$\rho = \frac{p}{RT}$$

Potential and Kinetic Energies

The total stored energy per unit mass:

$$e = \hat{u} + \frac{1}{2}V^2 + gz$$

- ▶ the internal energy is a function of temperature
- ▶ the potential and kinetic energies are kinematic quantities

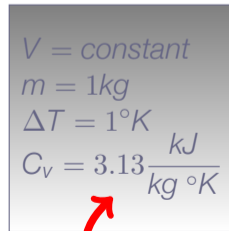
State Relations for Gases

The perfect gas law:

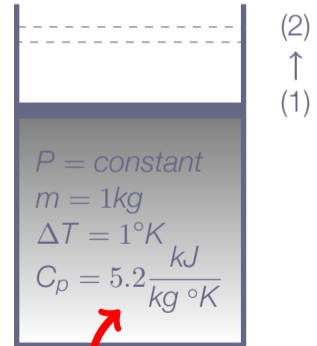
$$p = \rho RT$$

where R is the gas constant

$$R = C_p - C_v$$



3.13kJ



5.2kJ

State Relations for Gases

The ideal gas law requires: $\hat{u} = \hat{u}(T)$ and thus

specific heat (constant volume):

$$C_v = \left(\frac{\partial \hat{u}}{\partial T} \right)_\rho = \frac{d\hat{u}}{dT} = C_v(T)$$



State Relations for Gases

specific heat (constant pressure):

$$h = \hat{u} + \frac{p}{\rho} = \hat{u} + RT = h(T)$$

$$C_p = \left(\frac{\partial h}{\partial T} \right)_p = \frac{dh}{dT} = C_p(T)$$

ratio of specific heats:

$$\gamma = \frac{C_p}{C_v} \geq 1$$



State Relations for Gases

$$C_v = \frac{R}{\gamma - 1}$$

$$C_p = \frac{\gamma R}{\gamma - 1}$$



Speed of Sound

Speed of sound plays an important role when compressible effects are important (Chapter 9)

$$a^2 = \left(\frac{\partial p}{\partial \rho} \right)_s$$

$$\tau_s = \frac{1}{\rho} \left(\frac{\partial \rho}{\partial p} \right)_s \Rightarrow a = \sqrt{\frac{1}{\rho \tau_s}}$$

where τ_s is the fluid compressibility

for an ideal gas:

$$a = \sqrt{\gamma RT}$$

Vapor Pressure

"the pressure at which a liquid boils and is in equilibrium with its own vapor"

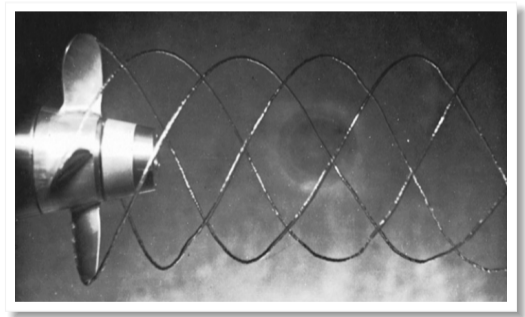
Vapor pressure for water:

T [°C]	vapor pressure [Pa]
20	2340
100	101300

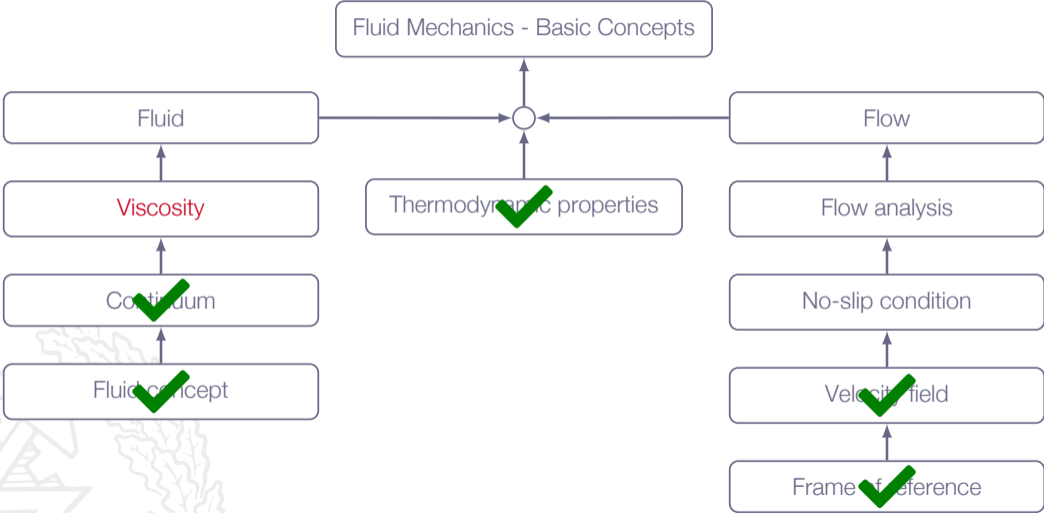


Vapor Pressure

- ▶ If the pressure in a liquid gets lower than the vapor pressure, vapor bubbles will appear in the liquid
- ▶ If the pressure drops below the vapor pressure due to the flow itself we get cavitation



Roadmap - Introduction to Fluid Mechanics





Viscosity

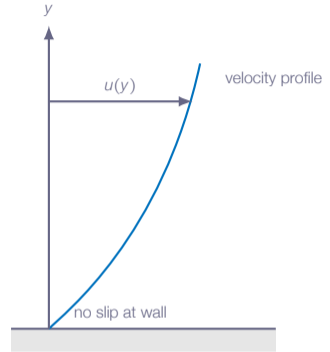
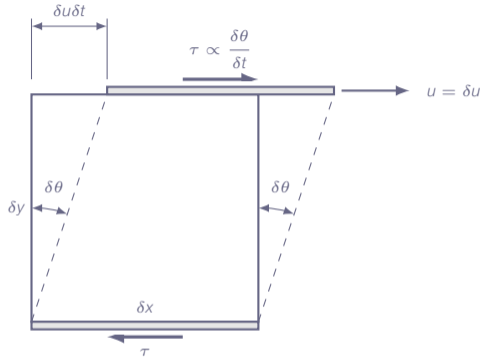
Viscosity

"relates the local stresses in a moving fluid to the strain rate of the fluid element"

"a quantitative measure of the fluid's resistance to flow"



Viscosity



$$\tau \propto \frac{\delta \theta}{\delta t}, \quad \tan \delta \theta = \frac{\delta u \delta t}{\delta y}$$

Viscosity

for infinitesimal changes:

$$\frac{d\theta}{dt} = \frac{du}{dy}$$

from before we know that $\tau \propto \frac{\delta\theta}{\delta t}$ and thus $\tau \propto \frac{d\theta}{dt}$

For newtonian fluids:

$$\tau = \mu \frac{d\theta}{dt} = \mu \frac{du}{dy}$$

where μ is the fluid viscosity

Viscosity

- ▶ Liquids have high viscosity that decreases with temperature
 - ▶ intermolecular forces decreases with temperature
- ▶ Gases have low viscosity that increases with temperature
 - ▶ increased temperature means increased molecular movement



Viscosity

Fluid	μ ($\text{kg m}^{-1} \text{s}^{-1}$)	ρ (kg m^{-3})	ν ($\text{m}^2 \text{s}^{-1}$)
Hydrogen	8.8 E-06	8.400 E-02	1.05 E-04
Air	1.8 E-05	1.200 E+00	1.51 E-05
Gasoline	2.9 E-04	6.800 E+02	4.22 E-07
Water	1.0 E-03	9.980 E+02	1.01 E-06
Mercury	1.5 E-03	1.358 E+04	1.16 E-07
SAE-30 Oil	2.9 E-02	8.910 E+02	3.25 E-04
Glycerin	1.5 E+00	1.264 E+03	1.18 E-03

Note! there are two different viscosities in the table (dynamic viscosity μ and kinematic viscosity $\nu = \mu/\rho$)

Viscosity

Inviscid flows: flows where viscous forces are negligible

Viscous flows: flows where viscous forces are important



Reynolds number

$$Re = \frac{\rho V L}{\mu}$$

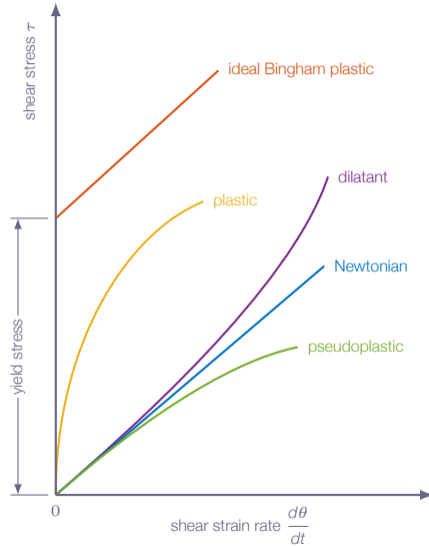
- ▶ Non-dimensional number that relates viscous forces to inertial forces
- ▶ Very important parameter in fluid mechanics
- ▶ V and L are characteristic velocity and length scales of the flow

Reynolds number

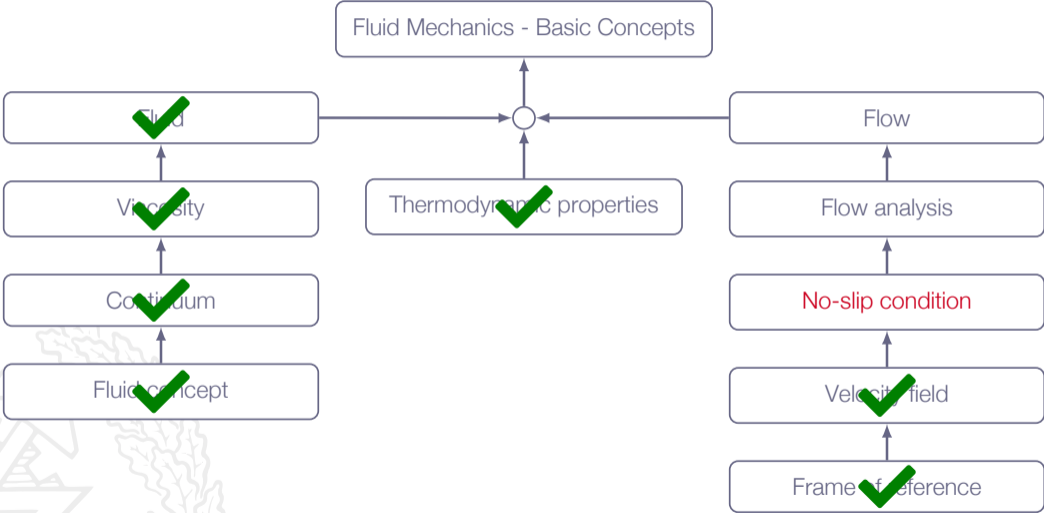
Reynolds number	flow description
low	viscous, creeping motion (inertial forces negligible)
moderate	laminar flow
high	turbulent flow



Non-Newtonian Fluids



Roadmap - Introduction to Fluid Mechanics



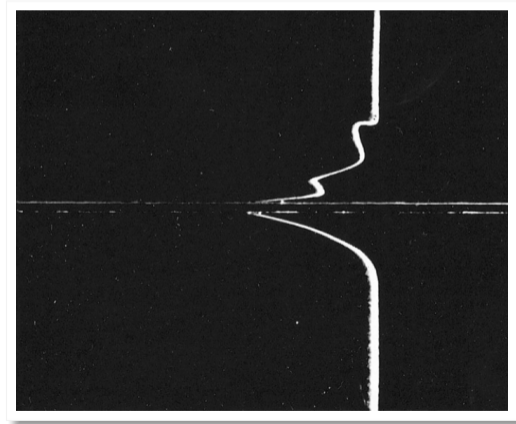
No Slip/No Temperature Jump

"When a fluid flow is bounded by a solid surface, molecular interactions cause the fluid in contact with the surface to seek momentum and energy equilibrium with that surface"

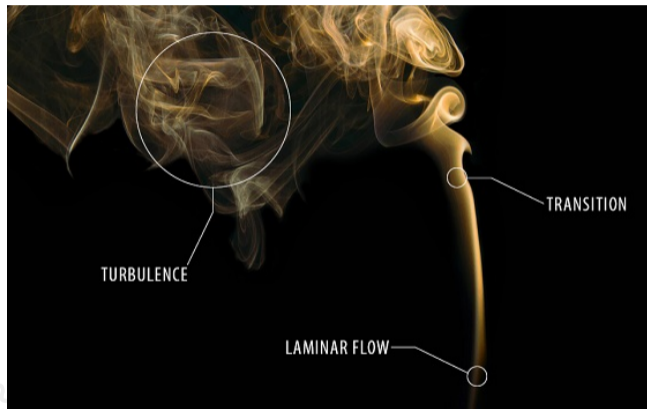


No Slip/No Temperature Jump

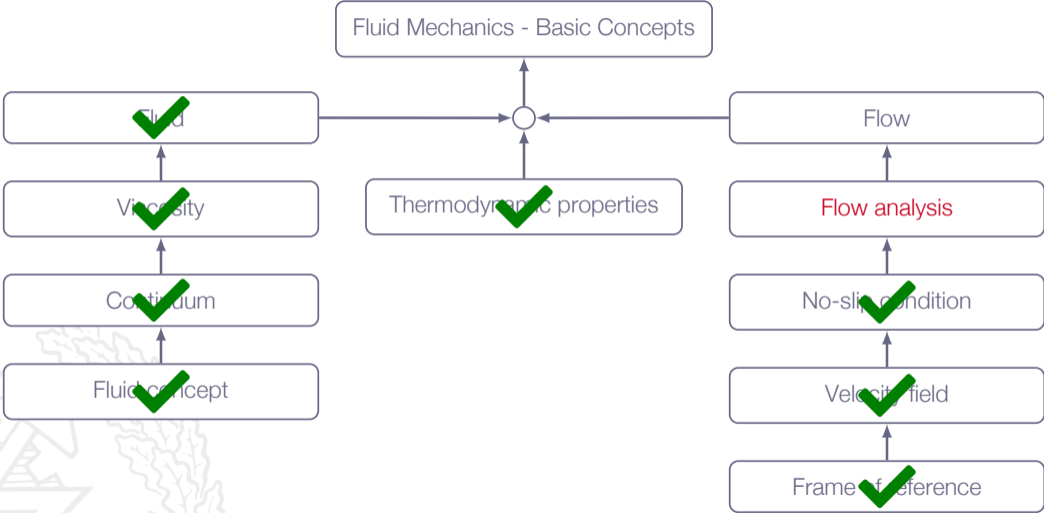
At a solid wall, the fluid will have the velocity and temperature of the wall



Laminar/Turbulent Flow



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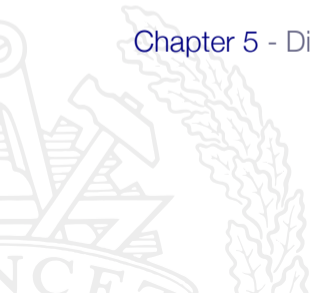


Flow Analysis

Chapter 3 - Control-volume (integral) approach

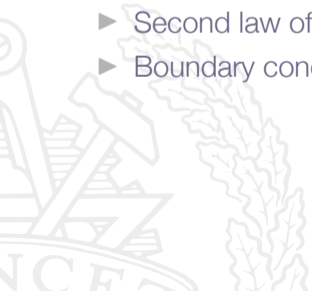
Chapter 4 - Infinitesimal system (differential) approach

Chapter 5 - Dimensional analysis approach



Flow Analysis

- ▶ Conservation of mass (continuity)
- ▶ Conservation of momentum (Newton's second law)
- ▶ Conservation of energy (first law of thermodynamics)
- ▶ State relation (for example the ideal gas law)
- ▶ Second law of thermodynamics
- ▶ Boundary conditions



Flow Visualization

Streamline

- ▶ a line that is tangent to the velocity vector everywhere at an instant in time

Pathline

- ▶ the actual path traversed by a fluid particle

Streakline

- ▶ the locus of particles that have earlier passed through a prescribed point

Timeline

- ▶ a line formed by a set of particles at a given instant



Flow Visualization

Streamline

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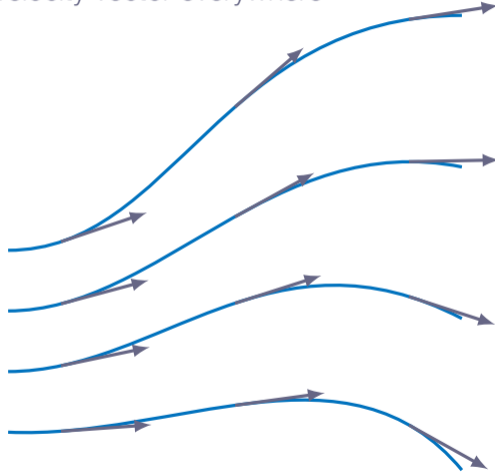
Timeline

- ▶ a line formed by a set of particles at a given instant

Note! In a steady-state flow, streamlines, pathlines and streaklines are identical

Streamline

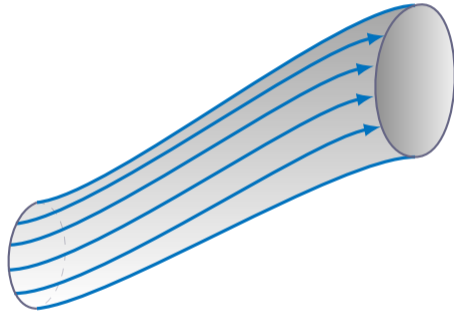
Tangent to flow velocity vector everywhere



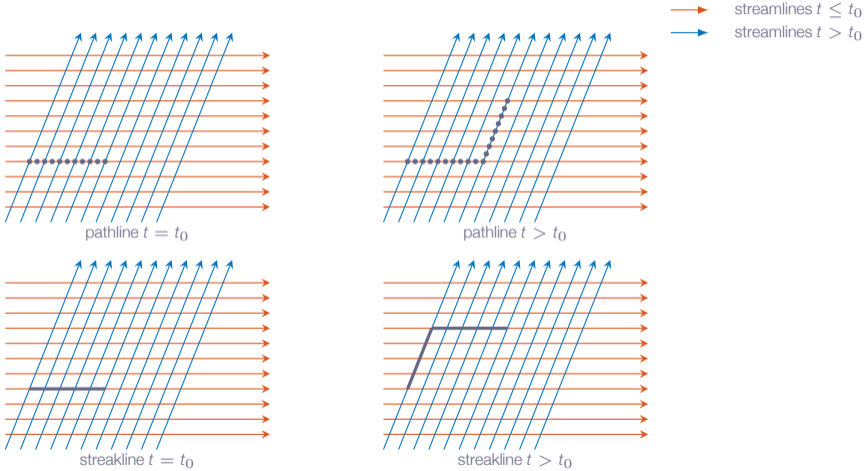
Streamtube

"Constructed" from individual streamlines

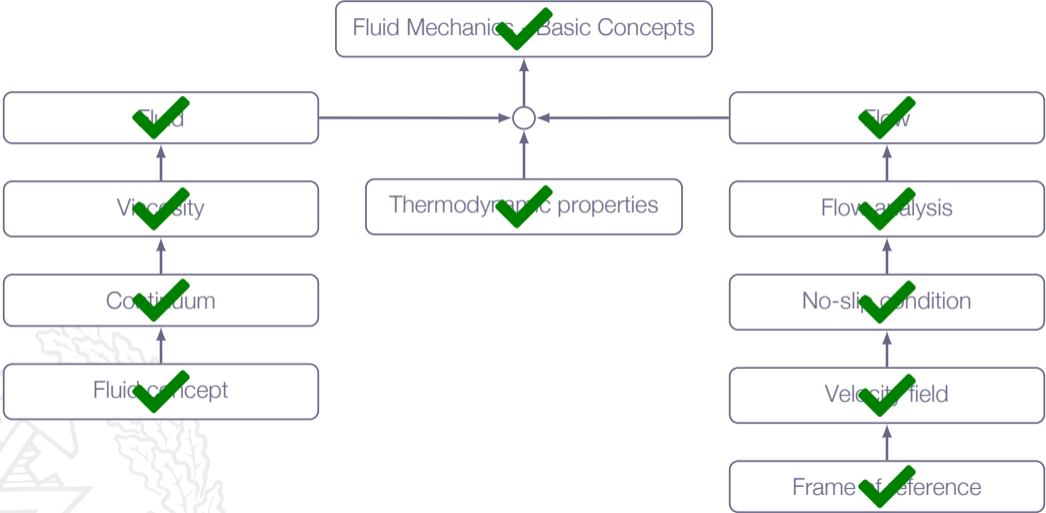
No flow across streamtube "walls" (by definition)



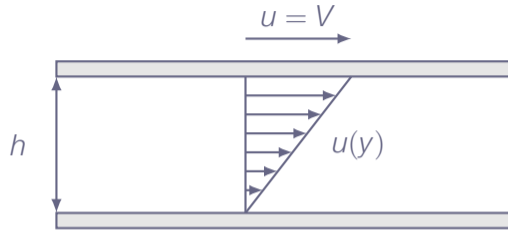
Pathline vs Streakline



Roadmap - Introduction to Fluid Mechanics

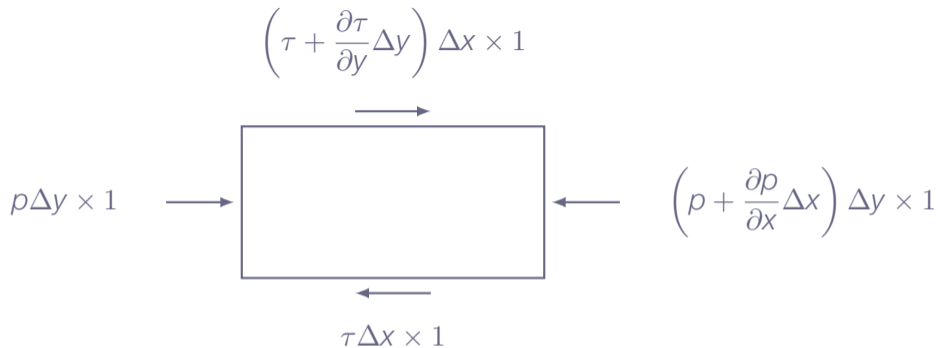


Example - Flow Between Plates



- ▶ No acceleration
- ▶ No pressure gradients
- ▶ two-dimensional flow

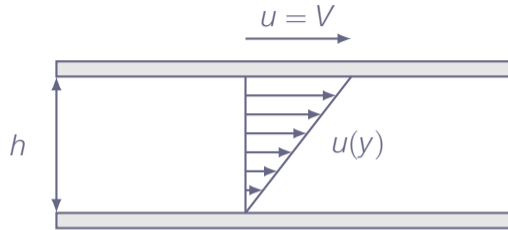
Example - Flow Between Plates



$$\sum F_x = p \Delta y - \left(p + \frac{\partial p}{\partial x} \Delta x\right) \Delta y + \left(\tau + \frac{\partial \tau}{\partial y} \Delta y\right) \Delta x - \tau \Delta x = 0$$

$$\frac{\partial \tau}{\partial y} = \frac{\partial p}{\partial x} = 0 \Rightarrow \tau = \text{const}$$

Example - Flow Between Plates



$$\frac{du}{dy} = \frac{\tau}{\mu} = \text{const}$$

$$u = a + by$$

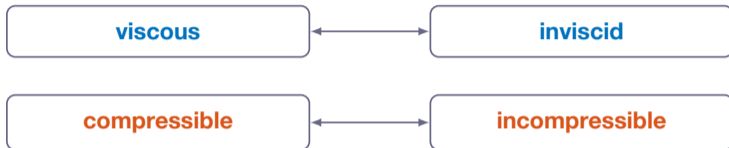
$$\begin{cases} y = 0 \Rightarrow u = 0 \\ y = h \Rightarrow u = V \end{cases}$$

$$u = \frac{V}{h}y$$

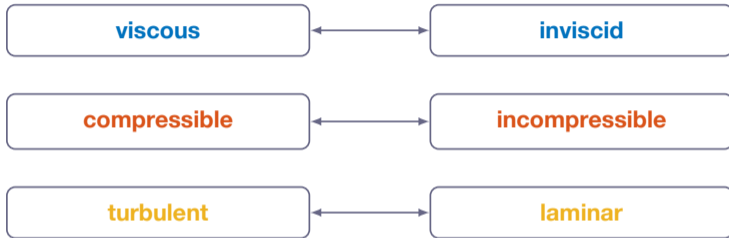
Flow Categories



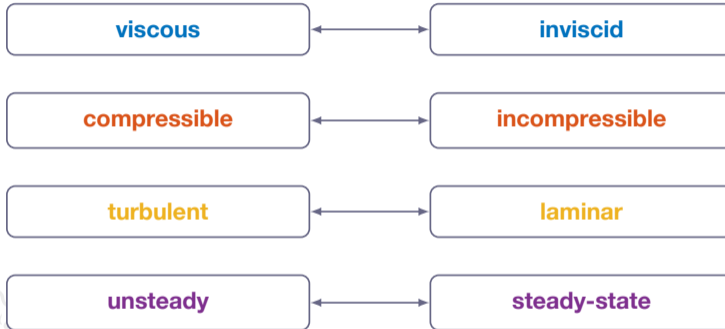
Flow Categories



Flow Categories



Flow Categories



Flow Categories

