Fluid Mechanics - MTF053

Lecture 2

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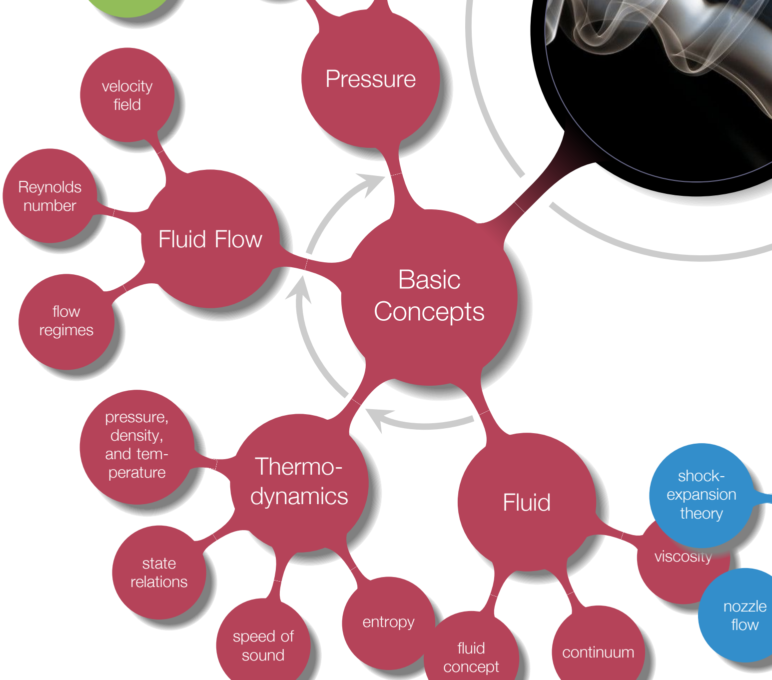
Chapter 1 - Introduction

Overview


Pressure
velocity field
Reynolds number
Fluid Flow
flow regimes
Basic Concepts
pressure, density, and tem-perature
Thermo-dynamics
state relations
speed of sound
entropy
Fluid
fluid concept
continuum
viscosity
shock-expansion theory
nozzle flow

Learning Outcomes

1 **Explain** the difference between a fluid and a solid in terms of forces and deformation

2 **Understand** and be able to explain the viscosity concept

3 **Define** the Reynolds number

5 **Explain** the difference between Lagrangian and Eulerian frame of reference and know when to use which approach

7 **Explain** the concepts: streamline, pathline and streakline

8 **Understand** and be able to **explain** the concept shear stress

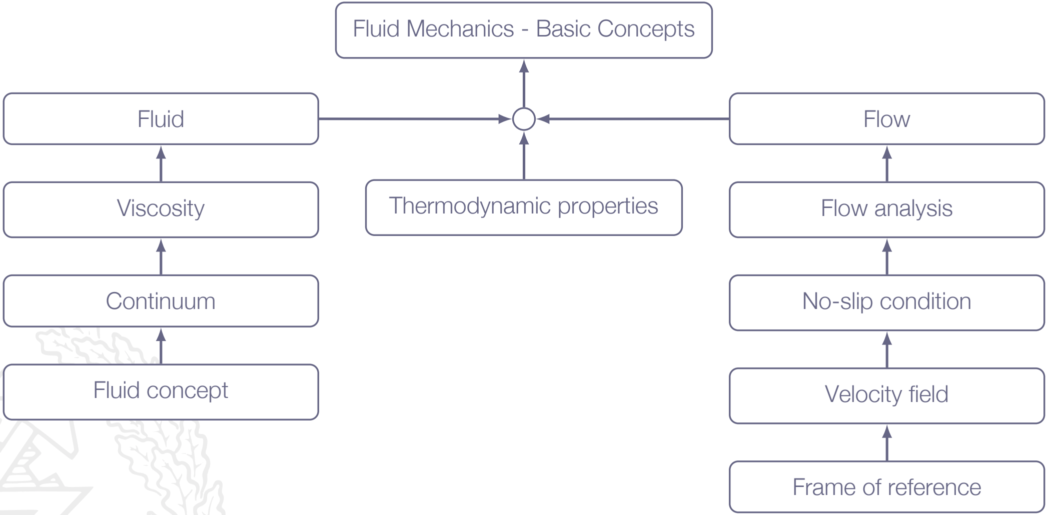
9 **Explain** how to do a force balance for fluid element (forces and pressure gradients)

10 **Understand and explain** buoyancy and cavitation

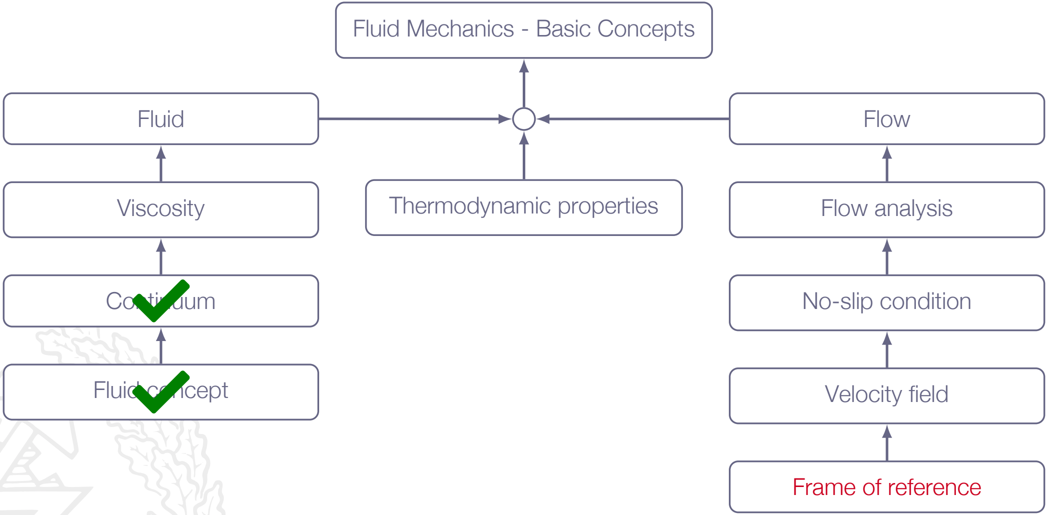
16 **Understand** and **explain** the concept Newtonian fluid

in this lecture we will find out what a fluid flow is

Roadmap - Introduction to Fluid Mechanics



Roadmap - Introduction to Fluid Mechanics



Frame of Reference

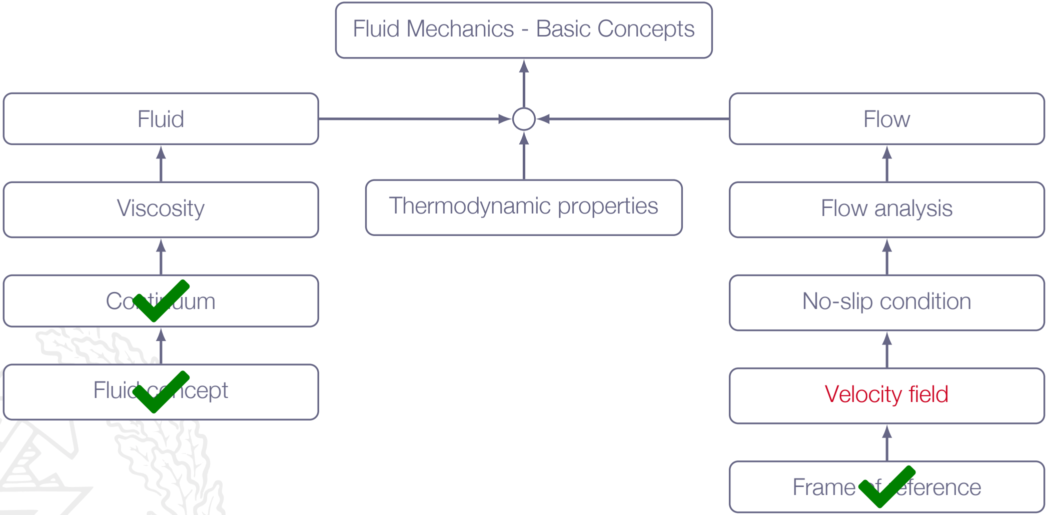
Eulerian Frame of Reference

fluid properties as function of position and time

Lagrangian Frame of Reference

follows a system in time and space

Roadmap - Introduction to Fluid Mechanics



Properties of the Velocity Field

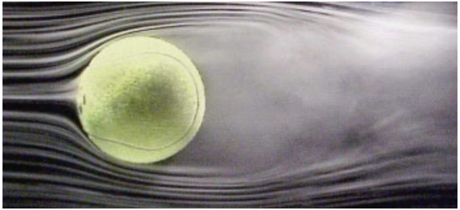
The fluid velocity is a function of position and time

Three components u, v, and w (one in each spatial direction)

$$\mathbf{V}(x,y,z,t) = u(x,y,z,t)\mathbf{e}_x + v(x,y,z,t)\mathbf{e}_y + w(x,y,z,t)\mathbf{e}_z$$

Properties of the Velocity Field

Acceleration:

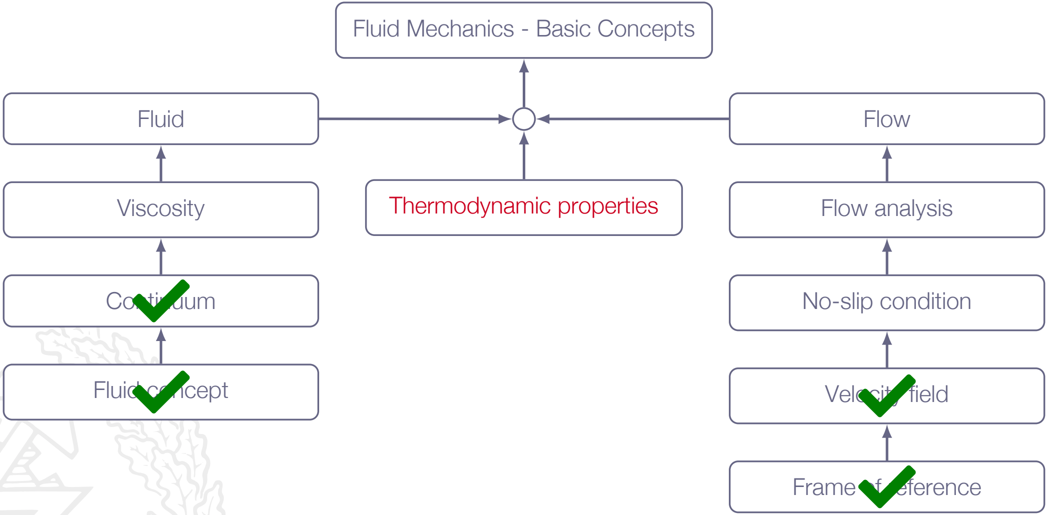


$$\mathbf{V}(x,y,z,t) = u(x,y,z,t)\mathbf{e}_x + v(x,y,z,t)\mathbf{e}_y + w(x,y,z,t)\mathbf{e}_z$$

$$\mathbf{a} = \frac{d\mathbf{V}}{dt} = \frac{\partial \mathbf{V}}{\partial t} + \left(\frac{\partial \mathbf{V}}{\partial x}\right)\left(\frac{\partial x}{\partial t}\right) + \left(\frac{\partial \mathbf{V}}{\partial y}\right)\left(\frac{\partial y}{\partial t}\right) + \left(\frac{\partial \mathbf{V}}{\partial z}\right)\left(\frac{\partial z}{\partial t}\right)$$

$$\frac{d\mathbf{V}}{dt} = \frac{\partial \mathbf{V}}{\partial t} + u\frac{\partial \mathbf{V}}{\partial x} + v\frac{\partial \mathbf{V}}{\partial y} + w\frac{\partial \mathbf{V}}{\partial z}$$

Roadmap - Introduction to Fluid Mechanics



Thermodynamic Properties

Thermodynamic properties describe the state of a system, i.e., a collection of matter of fixed identity which interacts with its surroundings

In this course, the system will be a small fluid element, and all properties will be assumed to be continuum properties of the flow field

Thermodynamic Properties

Pressure: p (Pa)
Density: ρ (kg/m^3)
Temperature: T (K)

most common properties

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most common properties

Internal energy: $\hat{u}$ (J/kg)
Enthalpy: $h = \hat{u} + p/\rho$ (J/kg)
Entropy: s $(J/(kg\,K))$
Specific heats: C_p and C_v $(J/(kg\,K))$

work, heat, and energy balances

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work, heat, and energy balances

Viscosity: μ $(kg/(m\,s))$
Thermal conductivity: k $(W/(m\,K))$

friction and heat conduction

Thermodynamic Properties

For a single-phase substance, two basic properties are sufficient to get the values of all others

$$\rho = \rho(p,T),\ h = h(p,T),\ \mu = \mu(p,T)$$

In the following it will be assumed that all thermodynamic properties exists as point functions in a flowing fluid ($\rho = \rho(x,y,z,t)$)

- large enough number of molecules $\Rightarrow$ **continuum**
- any changes in thermodynamic conditions are faster than the flow time scale $\Rightarrow$ **equilibrium**

Primary Thermodynamic Properties

Pressure

The compression stress at a point in a static fluid

A fluid flow is often driven by pressure gradients

If the pressure drops below the vapor pressure in a liquid, vapor bubbles will form

Primary Thermodynamic Properties

Temperature

Related to internal energy

Large temperature differences $\Rightarrow$ heat transfer may be important

Primary Thermodynamic Properties

Density

Mass per unit volume

Nearly constant in liquids (incompressible) - for water, the density increases about one percent for a pressure increase by a factor of 220

Not constant for gases

$$\rho = \frac{p}{RT}$$

Potential and Kinetic Energies

The total stored energy per unit mass:

$$e = \hat{u} + \frac{1}{2}V^2 + gz$$

the internal energy is a function of temperature

the potential and kinetic energies are kinematic quantities

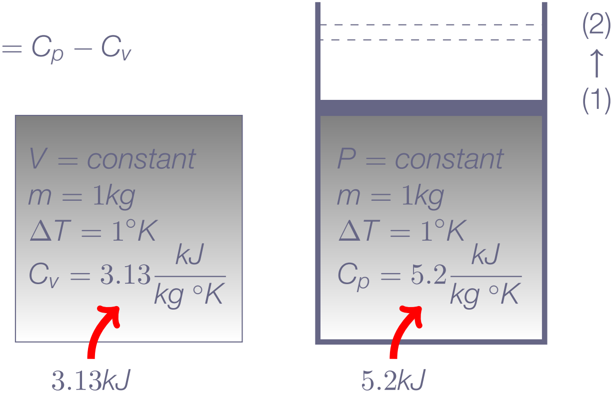
State Relations for Gases

The perfect gas law:

$$p = \rho R T$$

where R is the gas constant

$$R = C_p - C_v$$



State Relations for Gases

The ideal gas law requires: $\hat{u} = \hat{u}(T)$ and thus

specific heat (constant volume):

$$C_v = \left(\frac{\partial \hat{u}}{\partial T}\right)_\rho = \frac{d\hat{u}}{dT} = C_v(T)$$

State Relations for Gases

specific heat (constant pressure):

$$h = \hat{u} + \frac{p}{\rho} = \hat{u} + RT = h(T)$$

$$C_p = \left(\frac{\partial h}{\partial T}\right)_p = \frac{dh}{dT} = C_p(T)$$

ratio of specific heats:

$$\gamma = \frac{C_p}{C_v} \geq 1$$

State Relations for Gases

$$C_v = \frac{R}{\gamma - 1}$$

$$C_p = \frac{\gamma R}{\gamma - 1}$$

Speed of Sound

Speed of sound plays an important role when compressible effects are important (Chapter 9)

$$a^2 = \left(\frac{\partial p}{\partial \rho}\right)_s$$

$$\tau_s = \frac{1}{\rho}\left(\frac{\partial \rho}{\partial p}\right)_s \Rightarrow a = \sqrt{\frac{1}{\rho \tau_s}}$$

where τ_s is the fluid **compressibility**

for an ideal gas:

$$\boxed{a = \sqrt{\gamma R T}}$$

Vapor Pressure

"the pressure at which a liquid boils and is in equilibrium with its own vapor"

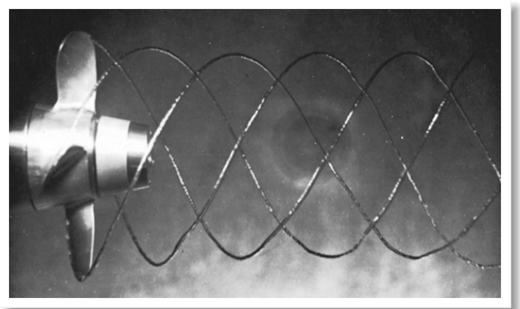
Vapor pressure for water:

$T\ [^{\circ}C]$	vapor pressure $[Pa]$
20	2340
100	101300

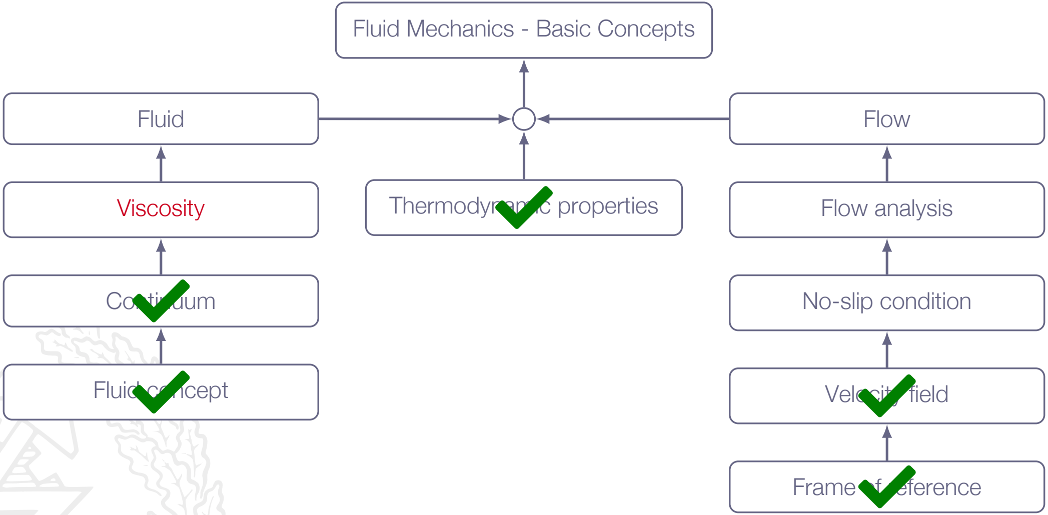
Vapor Pressure

If the pressure in a liquid gets lower than the vapor pressure, vapor bubbles will appear in the liquid

If the pressure drops below the vapor pressure due to the flow itself we get cavitation



Roadmap - Introduction to Fluid Mechanics



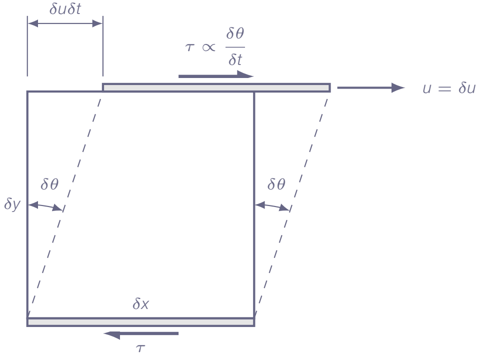
Viscosity

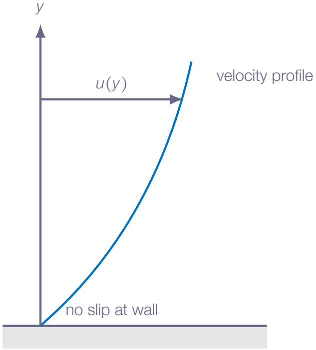
Viscosity

”relates the local stresses in a moving fluid to the strain rate of the fluid element”

”a quantitative measure of the fluid’s resistance to flow”

Viscosity





$$\tau \propto \frac{\delta\theta}{\delta t}, \; \tan\delta\theta = \frac{\delta u \delta t}{\delta y}$$

Viscosity

for infinitesimal changes:

$$\frac{d\theta}{dt} = \frac{du}{dy}$$

from before we know that $\tau \propto \frac{\delta\theta}{\delta t}$ and thus $\tau \propto \frac{d\theta}{dt}$

For Newtonian fluids:

$$\boxed{\tau = \mu\frac{d\theta}{dt} = \mu\frac{du}{dy}}$$

where μ is the fluid viscosity

Viscosity

Liquids have high viscosity that decreases with temperature

- intermolecular forces decreases with temperature

Gases have low viscosity that increases with temperature

- increased temperature means increased molecular movement

Viscosity

Fluid	$\mu \ (kg\ m^{-1}\ s^{-1})$	$\rho \ (kg\ m^{-3})$	$\nu \ (m^2\ s^{-1})$
Hydrogen	8.8 E-06	8.400 E-02	1.05 E-04
Air	1.8 E-05	1.200 E+00	1.51 E-05
Gasoline	2.9 E-04	6.800 E+02	4.22 E-07
Water	1.0 E-03	9.980 E+02	1.01 E-06
Mercury	1.5 E-03	1.358 E+04	1.16 E-07
SAE-30 Oil	2.9 E-02	8.910 E+02	3.25 E-04
Glycerin	1.5 E+00	1.264 E+03	1.18 E-03

Note! there are two different viscosities in the table (dynamic viscosity μ and kinematic viscosity $\nu = \mu/\rho$)

Viscosity

Inviscid flows: flows where viscous forces are negligible

Viscous flows: flows where viscous forces are important

Reynolds number

$$\boxed{Re = \frac{\rho V L}{\mu}}$$

Non-dimensional number that relates viscous forces to inertial forces

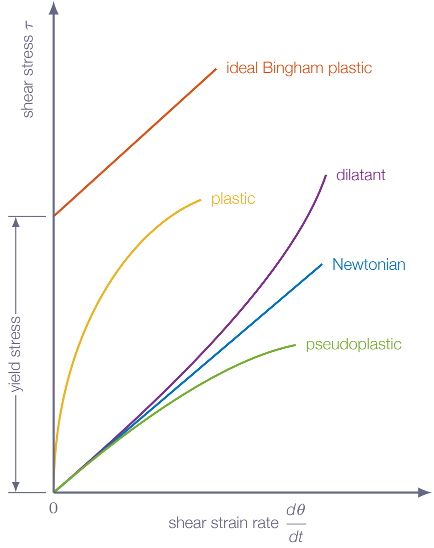
Very important parameter in fluid mechanics

V and L are characteristic velocity and length scales of the flow

Reynolds number

Reynolds number	flow description
low	viscous, creeping motion (inertial forces negligible)
moderate	laminar flow
high	turbulent flow

Non-Newtonian Fluids



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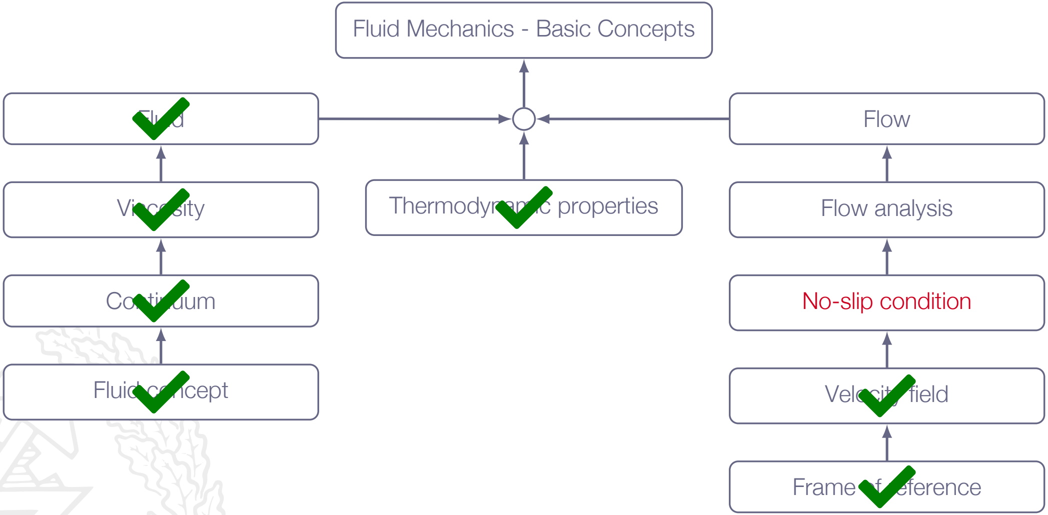
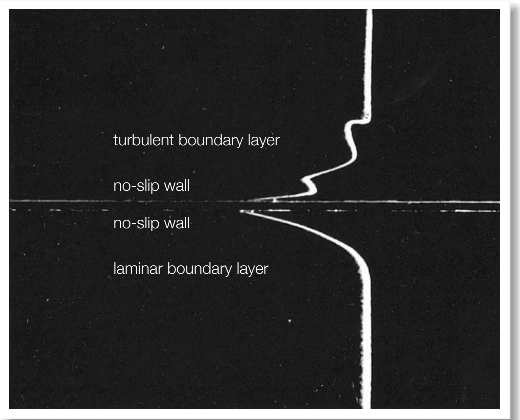


No Slip/No Temperature Jump

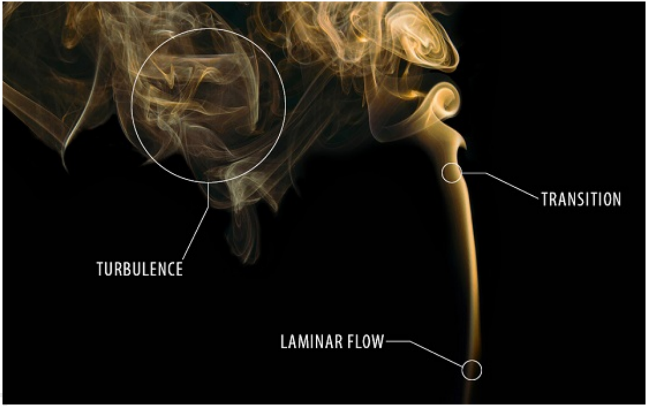
"When a fluid flow is bounded by a solid surface, molecular interactions cause the fluid in contact with the surface to seek momentum and energy equilibrium with that surface"

No Slip/No Temperature Jump

At a solid wall, the fluid will have the velocity and temperature of the wall



Laminar/Turbulent Flow



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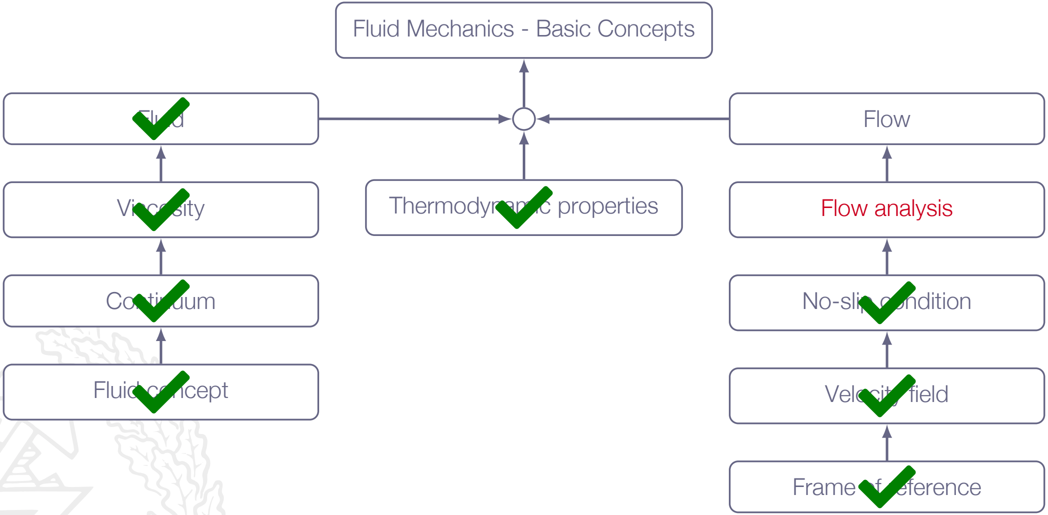

Flow Analysis

Chapter 3 - Control-volume (integral) approach

Chapter 4 - Infinitesimal system (differential) approach

Chapter 5 - Dimensional analysis approach

Flow Analysis

1. Conservation of mass (continuity)
2. Conservation of momentum (Newton's second law)
3. Conservation of energy (first law of thermodynamics)
4. State relation (for example the ideal gas law)
5. Second law of thermodynamics
6. Boundary conditions

Flow Visualization

Streamline
: a line that is tangent to the velocity vector everywhere at an instant in time

Pathline
: the actual path traversed by a fluid particle

Streakline
: the locus of particles that have earlier passed through a prescribed point

Timeline
: a line formed by a set of particles at a given instant

Flow Visualization

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: a line that is tangent to the velocity vector everywhere at an instant in time

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Timeline
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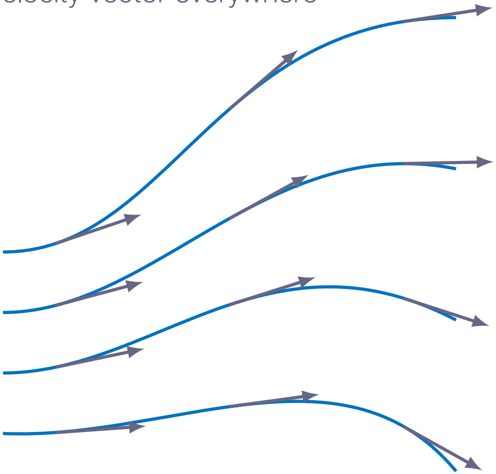
Note! In a steady-state flow, streamlines, pathlines and streaklines are identical

Streamline

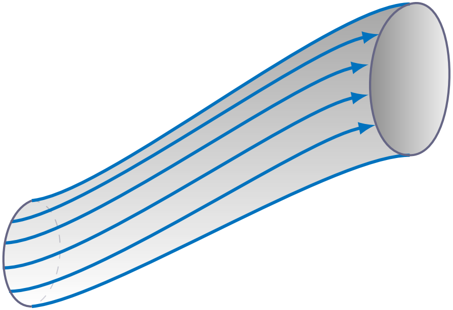
Tangent to flow velocity vector everywhere



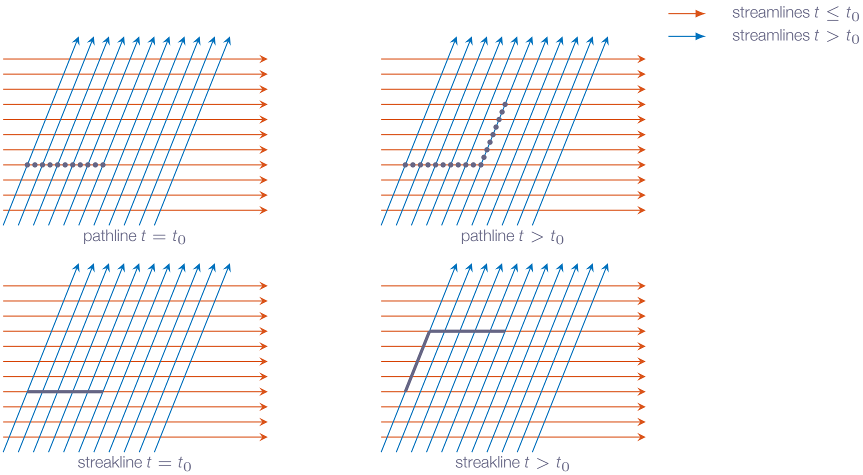
Streamtube

"Constructed" from individual streamlines

No flow across streamtube "walls" (by definition)



Pathline vs Streakline



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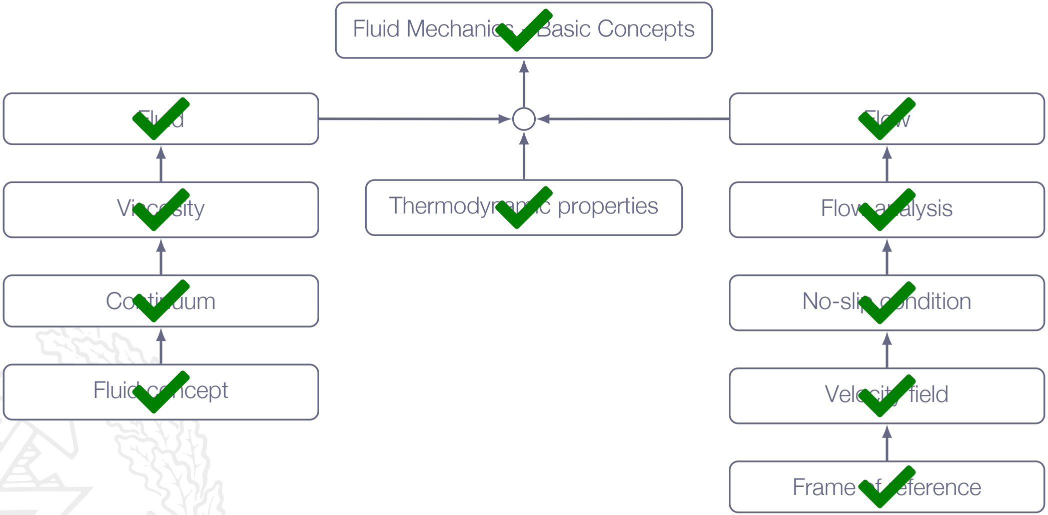
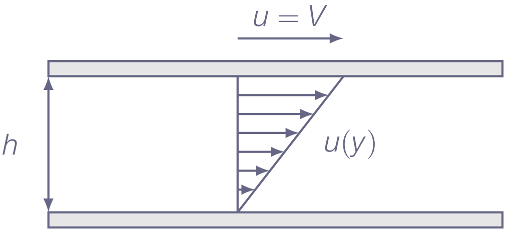


Example - Flow Between Plates



No acceleration

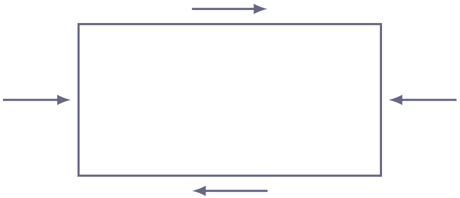
No pressure gradients

two-dimensional flow

Example - Flow Between Plates

$$\left(\tau + \frac{\partial \tau}{\partial y}\Delta y\right)\Delta x \times 1$$

$$p\Delta y \times 1$$



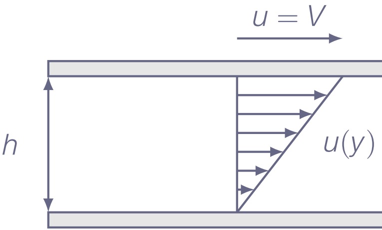
$$\left(p + \frac{\partial p}{\partial x}\Delta x\right)\Delta y \times 1$$

$$\tau \Delta x \times 1$$

$$\sum F_x = p\Delta y - \left(p + \frac{\partial p}{\partial x}\Delta x\right)\Delta y + \left(\tau + \frac{\partial \tau}{\partial y}\Delta y\right)\Delta x - \tau \Delta x = 0$$

$$\frac{\partial \tau}{\partial y} = \frac{\partial p}{\partial x} = 0 \Rightarrow \tau = const$$

Example - Flow Between Plates



$$\frac{du}{dy} = \frac{\tau}{\mu} = const$$

$$u = a + by$$

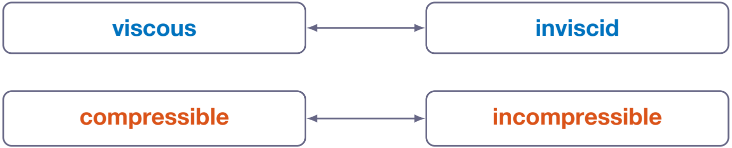
$$\begin{cases} y = 0 \Rightarrow u = 0 \\ y = h \Rightarrow u = V \end{cases}$$

$$u = \frac{V}{h} y$$

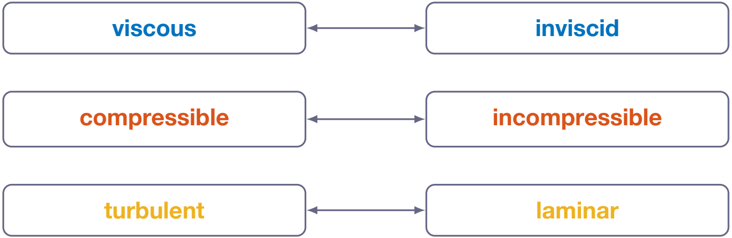
Flow Categories

viscous ⟷ **inviscid**

Flow Categories



Flow Categories



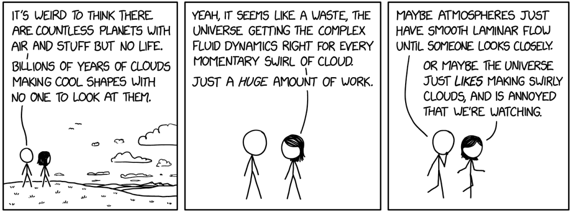
Flow Categories

viscous	⟷	**inviscid**
compressible	⟷	**incompressible**
turbulent	⟷	**laminar**
unsteady	⟷	**steady-state**

Flow Categories

viscous	↔	inviscid
compressible	↔	incompressible
turbulent	↔	laminar
unsteady	↔	steady-state
3D	↔	1D/2D

Clouds


IT'S WEIRD TO THINK THERE ARE COUNTLESS PLANETS WITH AIR AND STUFF BUT NO LIFE.
BILLIONS OF YEARS OF CLOUDS MAKING COOL SHAPES WITH NO ONE TO LOOK AT THEM.
YEAH, IT SEEMS LIKE A WASTE, THE UNIVERSE GETTING THE COMPLEX FLUID DYNAMICS RIGHT FOR EVERY MOMENTARY SWIRL OF CLOUD.
JUST A *HUGE* AMOUNT OF WORK.
MAYBE ATMOSPHERES JUST HAVE SMOOTH LAMINAR FLOW UNTIL SOMEONE LOOKS CLOSELY.
OR MAYBE THE UNIVERSE JUST *LIKES* MAKING SWIRLY CLOUDS, AND IS ANNOYED THAT WE'RE WATCHING.