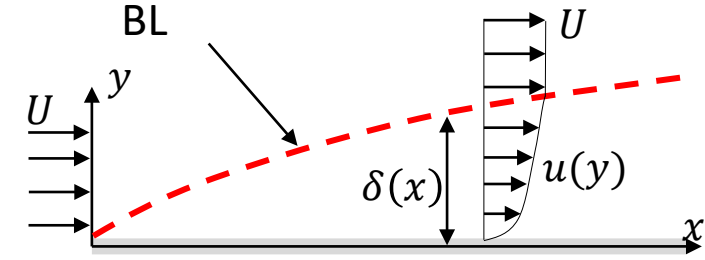


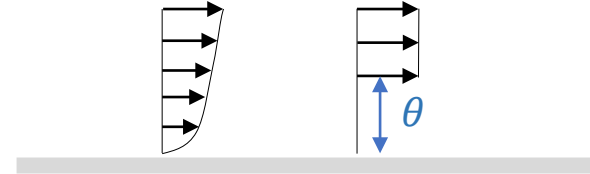
Exercise 12.

- Boundary Layer (BL) theory



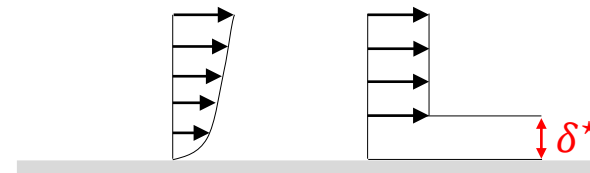
- Momentum thickness θ
 - Same linear momentum
 - Linear flow profile

$$\theta = \int_0^{\delta} \frac{u}{U} \left(1 - \frac{u}{U}\right) dy \quad \text{Eq. (7.3)}$$



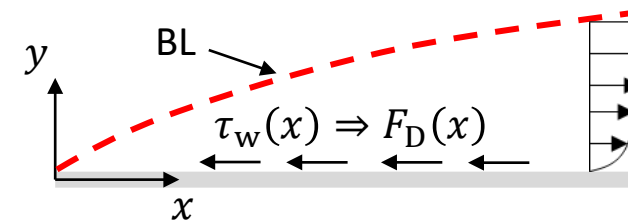
- Displacement thickness δ^*
 - Same mass flow rate
 - Linear flow profile

$$\delta^* = \int_0^{\delta} \left(1 - \frac{u}{U}\right) dy \quad \text{Eq. (7.12)}$$



- Skin friction coefficient c_f
 - Compare with friction coefficient for pipe flow

$$c_f = \frac{2\tau_w}{\rho U^2} \quad \text{Eq. (7.10), with } \tau_w = \rho U^2 \frac{d\theta}{dx} \quad \text{Eq. (7.5)}$$



Exercise 12.

- Karman flat plate – **Laminar flow (don't use this):**

$$\frac{u(x,y)}{U} \approx \left(\frac{2y}{\delta} - \frac{y^2}{\delta^2} \right) \text{ (parabolic) Eq. (7.6)}$$

- Blasius flat plate – **Laminar flow:**

$$\frac{u(x,y)}{U} = f'(\eta) \text{ (Blasius profile) Eq. (7.21)}$$

- Use Blasius for laminar flow, if nothing else is stated!
- Eq. (7.21) – (7.31), and Table 7.1

- Prandtl flat plate – **Turbulent flow:**

$$\left(\frac{u}{U} \right)_{\text{Turb}} \approx \left(\frac{y}{\delta} \right)^{1/7} \text{ (1/7-rule) Eq. (7.39)}$$

- Eq. (7.39) – (7.49)

Exercise 12.

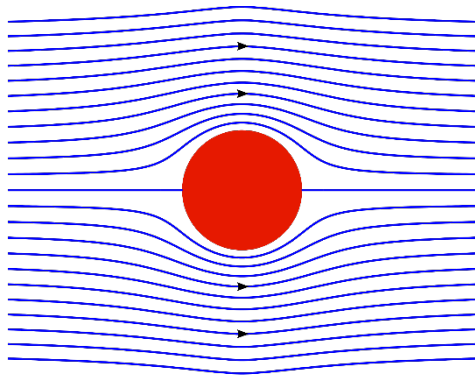
- **Laminar flow** (Blasius)

$$C_D = \frac{F_D}{\frac{\rho}{2} U^2 bL} = \frac{1.328}{\text{Re}_L^{1/2}} \quad \text{Eq. (7.27)}$$

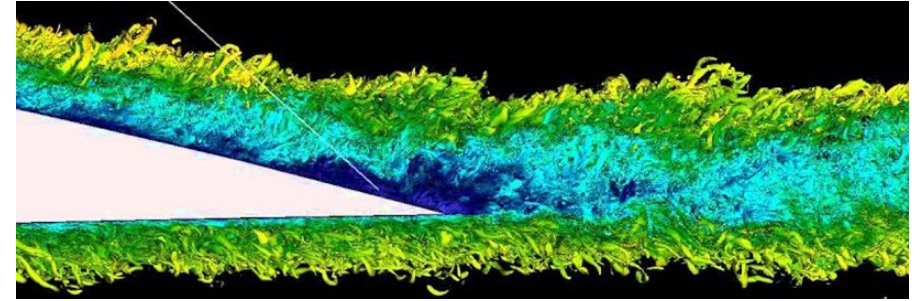
- Transition to turbulence $\text{Re}_{\text{trans}} = 5\text{E}5 - 1\text{E}6$ (if nothing else stated)
- **Turbulent flow** (Prandtl)

$$\text{Smooth wall: } C_D = \frac{0.031}{\text{Re}_L^{1/7}} \quad \text{Eq. (7.45)}$$

Rough wall: Use Fig. 7.6 and e.g (7.48) or (7.49)



Potential flow = stream function (Ψ), solve Laplace eqn + Bernoulli (Ch. 4)



DNS (**D**irect **N**umerical **S**imulation) = Navier-Stokes numerically (Ch. 4)

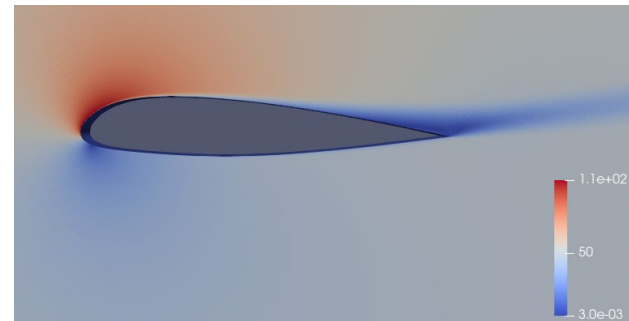


Fast and cheap, but not so accurate

Cost, computer resources

Slow and expensive, accurately resolved flow field

Potential flow + Von Karman (or similar boundary layer theory) → Streamlines can move away from the body, boundary layer thickness can be estimated, friction resistance can be estimated (Ch. 4 + Ch. 7)



RANS (**R**eynolds **A**veraged **N**avier-**S**tokes) = Solve the time-averaged Navier-Stokes + Boussinesq assumption

$$\tau_{turb} = -\rho \overline{u'v'} = \mu_t \left(\frac{\partial \bar{u}}{\partial y} + \frac{\partial \bar{v}}{\partial x} \right)$$