

# Compressible Flow - TME085

## Lecture 1

Niklas Andersson

Chalmers University of Technology  
Department of Mechanics and Maritime Sciences  
Division of Fluid Mechanics  
Gothenburg, Sweden

`niklas.andersson@chalmers.se`



# Overview



# Compressible Flow

*”Compressible flow (**gas dynamics**) is a branch of fluid mechanics that deals with flows having **significant changes in fluid density**”*

Wikipedia



# Gas Dynamics

*”... the study of **motion of gases** and its effects on physical systems ...”*

*”... based on the principles of **fluid mechanics** and **thermodynamics** ...”*

*”... gases flowing around or within physical objects at speeds comparable to the **speed of sound** ...”*

Wikipedia

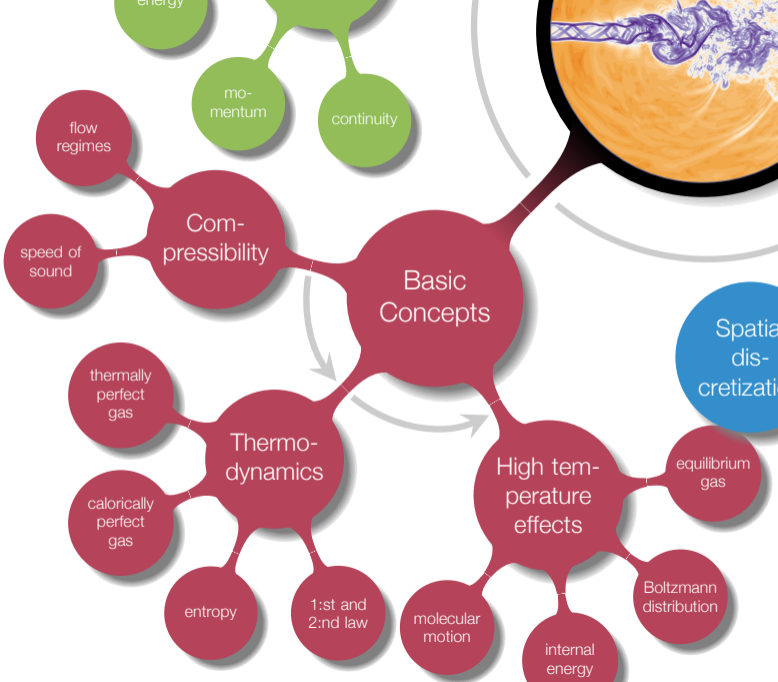


# Chapter 1

## Introduction



# Overview

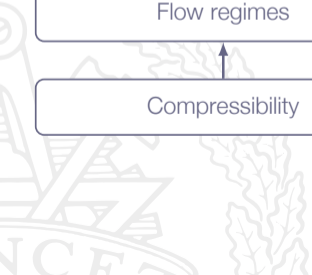
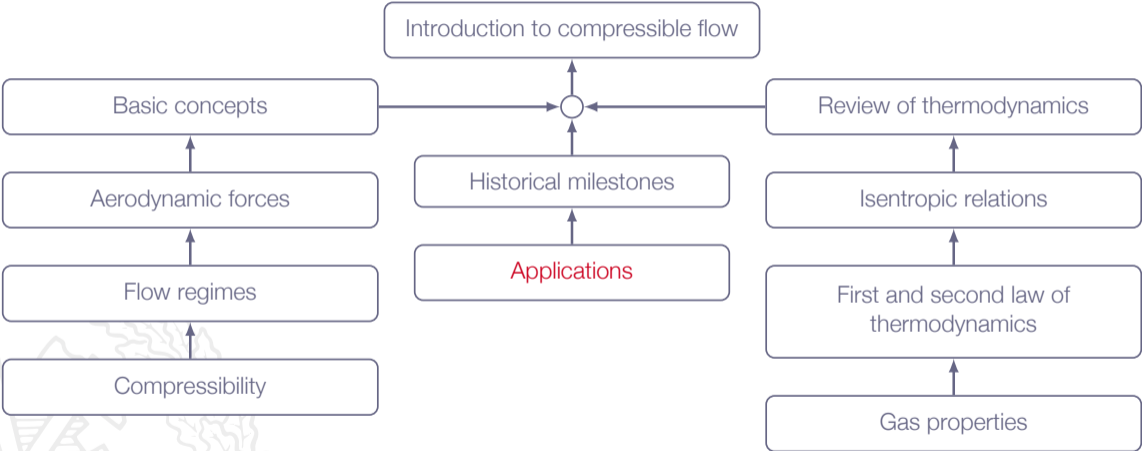


# Learning Outcomes

- 1 **Define** the concept of compressibility for flows
- 2 **Explain** how to find out if a given flow is subject to significant compressibility effects
- 3 **Describe** typical engineering flow situations in which compressibility effects are more or less predominant (e.g. Mach number regimes for steady-state flows)
- 6 **Define** the special cases of calorically perfect gas, thermally perfect gas and real gas and **explain** the implication of each of these special cases

*in this lecture we will find out what compressibility means and do a brief review of thermodynamics*

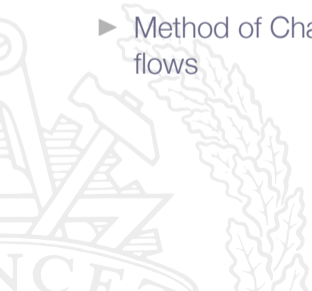
# Roadmap - Introduction to Compressible Flow





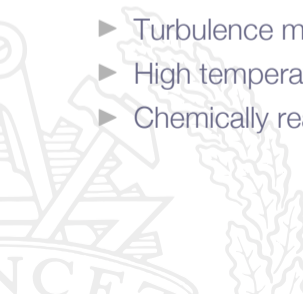
# Applications - Classical

- ▶ Treatment of calorically perfect gas
- ▶ Exact solutions of inviscid flow in 1D
- ▶ Shock-expansion theory for steady-state 2D flow
- ▶ Approximate closed form solutions to linearized equations in 2D and 3D
- ▶ Method of Characteristics (MOC) in 2D and axi-symmetric inviscid supersonic flows



# Applications - Modern

- ▶ Computational Fluid Dynamics (CFD)
- ▶ Complex geometries (including moving boundaries)
- ▶ Complex flow features (compression shocks, expansion waves, contact discontinuities)
- ▶ Viscous effects
- ▶ Turbulence modeling
- ▶ High temperature effects (molecular vibration, dissociation, ionization)
- ▶ Chemically reacting flow (equilibrium & non-equilibrium reactions)



# Applications - Examples

## Turbo-machinery flows:

- ▶ Gas turbines, steam turbines, compressors
- ▶ Aero engines (turbojets, turbofans, turboprops)

## Aeroacoustics:

- ▶ Flow induced noise (jets, wakes, moving surfaces)
- ▶ Sound propagation in high speed flows

## External flows:

- ▶ Aircraft (airplanes, helicopters)
- ▶ Space launchers (rockets, re-entry vehicles)

## Internal flows:

- ▶ Nozzle flows
- ▶ Inlet flows, diffusers
- ▶ Gas pipelines (natural gas, bio gas)

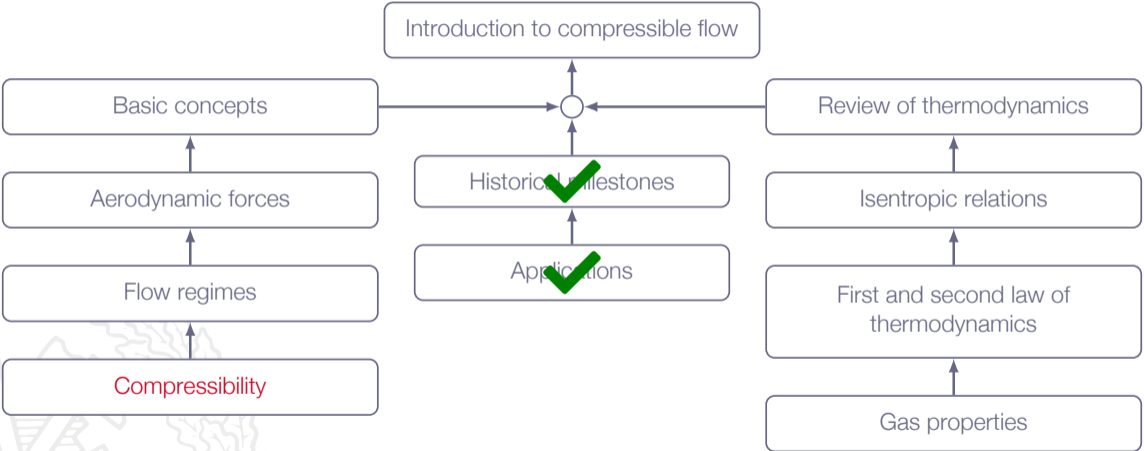
## Free-shear flows:

- ▶ High speed jets

## Combustion:

- ▶ Internal combustion engines (valve flow, in-cylinder flow, exhaust pipe flow, mufflers)
- ▶ Combustion induced noise (turbulent combustion)
- ▶ Combustion instabilities

# Roadmap - Introduction to Compressible Flow



# Chapter 1.2

## Compressibility

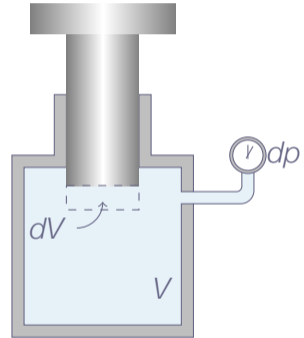


# Compressibility

$$\tau = -\frac{1}{\nu} \frac{\partial \nu}{\partial p}, \quad (\nu = \frac{1}{\rho})$$

Not really precise!

Is  $T$  held constant during the compression or not?



# Compressibility

Two fundamental cases:

## Constant temperature

Heat is cooled off to keep  $T$  constant inside the cylinder

## Adiabatic process

Thermal insulation prevents heat exchange



# Compressibility

Isothermal process:

$$\tau_T = -\frac{1}{\nu} \left( \frac{\partial \nu}{\partial \rho} \right)_T$$

Adiabatic reversible (*isentropic*) process:

$$\tau_S = -\frac{1}{\nu} \left( \frac{\partial \nu}{\partial \rho} \right)_S$$

Air at normal conditions:

$$\tau_T \approx 1.0 \times 10^{-5} \quad [m^2/N]$$

Water at normal conditions:

$$\tau_T \approx 5.0 \times 10^{-10} \quad [m^2/N]$$



# Compressibility

$$\tau = -\frac{1}{\nu} \frac{\partial \nu}{\partial p} \text{ where } \nu = \frac{1}{\rho} \text{ and thus}$$

$$\tau = -\rho \frac{\partial}{\partial p} \left( \frac{1}{\rho} \right) = -\rho \left( -\frac{1}{\rho^2} \right) \frac{\partial \rho}{\partial p} = \frac{1}{\rho} \frac{\partial \rho}{\partial p}$$

$$\tau_T = \frac{1}{\rho} \left( \frac{\partial \rho}{\partial p} \right)_T$$

$$\tau_S = \frac{1}{\rho} \left( \frac{\partial \rho}{\partial p} \right)_S$$

# Compressibility

## Definition of compressible flow:

If  $p$  changes with amount  $\Delta p$  over a characteristic length scale of the flow, such that the corresponding change in density, given by  $\Delta \rho \sim \rho \tau \Delta p$ , is **too large to be neglected**, the flow is compressible (*typically, if  $\Delta \rho / \rho > 0.05$* )

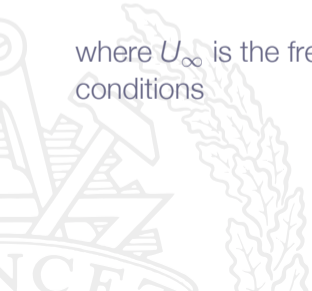
**Note!** Bernoulli's equation is restricted to incompressible flow, *i.e.* it is **not valid** for compressible flow!

# Compressibility - Mach Number

The freestream Mach number is defined as

$$M_{\infty} = \frac{U_{\infty}}{a_{\infty}}$$

where  $U_{\infty}$  is the freestream flow speed and  $a_{\infty}$  is the speed of sound at freestream conditions



# Compressibility

Assume incompressible flow and estimate the maximum pressure difference using

$$\Delta p \approx \frac{1}{2} \rho_{\infty} U_{\infty}^2$$

For air at normal conditions we have

$$\tau_T = \frac{1}{\rho} \left( \frac{\partial \rho}{\partial p} \right)_T = \frac{1}{\rho R T} = \frac{1}{\rho}$$

*(ideal gas law for perfect gas  $p = \rho R T$ )*

# Compressibility

Using the relations on previous slide we get

$$\frac{\Delta\rho}{\rho} \approx \tau_T \Delta p \approx \frac{1}{\rho_\infty} \frac{1}{2} \rho_\infty U_\infty^2 = \frac{\frac{1}{2} \rho_\infty U_\infty^2}{\rho_\infty R T_\infty}$$

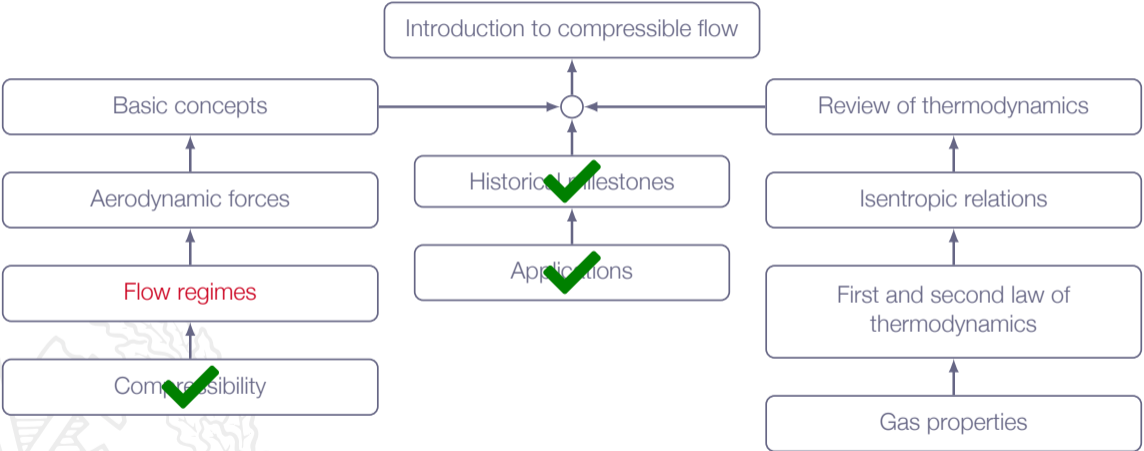
for a calorically perfect gas we have  $a = \sqrt{\gamma R T}$

which gives us  $\frac{\Delta\rho}{\rho} \approx \frac{\gamma U_\infty^2}{2a_\infty^2}$

now, using the definition of Mach number we get:

$$\frac{\Delta\rho}{\rho} \approx \frac{\gamma}{2} M_\infty^2$$

# Roadmap - Introduction to Compressible Flow



# Chapter 1.3

## Flow Regimes



# Flow Regimes

Incompressible

$$M_\infty < 0.1$$

Subsonic

$$M_\infty < 1 \text{ and } M < 1 \text{ everywhere}$$

Transonic

case 1:  $M_\infty < 1$  and  $M > 1$  locally  
case 2:  $M_\infty > 1$  and  $M < 1$  locally

Supersonic

$$M_\infty > 1 \text{ and } M > 1 \text{ everywhere}$$

Hypersonic

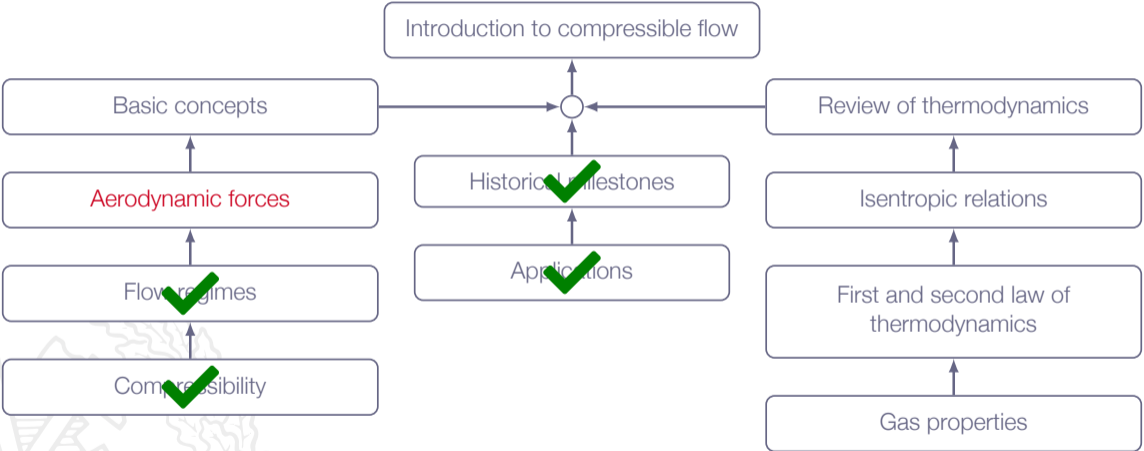
supersonic flow with high-temperature effects

Local Mach number  $M$  is based on local flow speed,  $U = |\mathbf{U}|$ , and local speed of sound,  $a$

Compressible



# Roadmap - Introduction to Compressible Flow

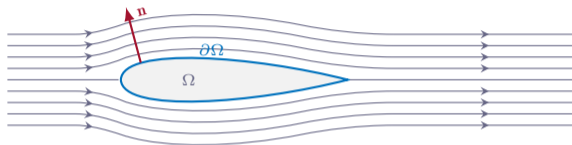


# Chapter 1.5

## Aerodynamic Forces



# Aerodynamic Forces



- $\Omega$  region occupied by body
- $\partial\Omega$  surface of body
- $\mathbf{n}$  outward facing unit normal vector

# Aerodynamic Forces

Overall forces on the body due to the flow

$$\mathbf{F} = \iint (-p\mathbf{n} + \boldsymbol{\tau} \cdot \mathbf{n})dS$$

where  $p$  is static pressure and  $\boldsymbol{\tau}$  is a stress tensor



# Aerodynamic Forces

**Drag** is the component of  $\mathbf{F}$  which is **parallel** with the freestream direction:

$$D = D_p + D_f$$

where  $D_p$  is drag due to pressure and  $D_f$  is drag due to friction

**Lift** is the component of  $\mathbf{F}$  which is **normal** to the free stream direction:

$$L = L_p + L_f$$

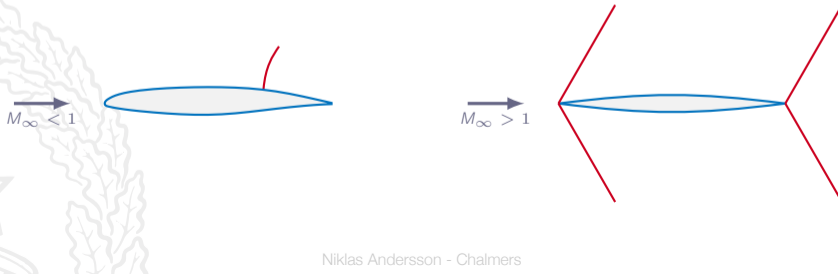
( $L_f$  is usually negligible)

# Aerodynamic Forces

Inviscid flow around slender body (*attached flow*)

- ▶ subsonic flow:  $D = 0$
- ▶ transonic or supersonic flow:  $D > 0$

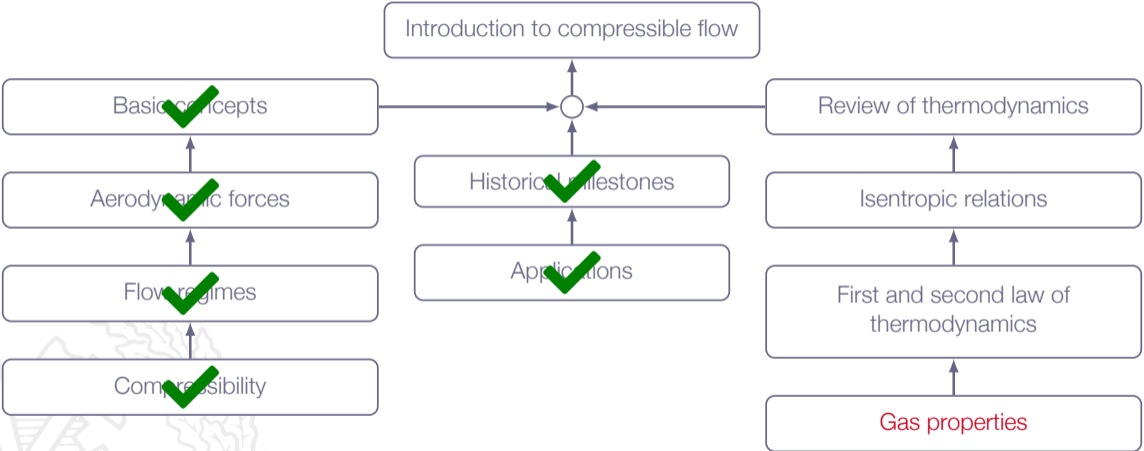
Explanation: **Wave drag**



# Aerodynamic Forces

- ▶ **Wave drag** is an **inviscid phenomena**, connected to the formation of compression shocks and entropy increase
- ▶ Viscous effects are present in all Mach regimes
- ▶ At transonic and supersonic conditions a particular phenomena named "shock/boundary-layer interaction" may appear
  - ▶ shocks trigger flow separation
  - ▶ usually leads to unsteady flow

# Roadmap - Introduction to Compressible Flow





# Chapter 1.4

## Review of Thermodynamics



# Thermodynamic Review

Compressible flow:

*” strong interaction between flow and thermodynamics ... ”*



# Perfect Gas

All intermolecular forces negligible

Only elastic collisions between molecules

$$p\nu = RT \text{ or } \frac{p}{\rho} = RT$$

where  $R$  is the gas constant  $[R] = J/kgK$

Also,  $R = R_{univ}/M$  where  $M$  is the molecular weight of gas molecules (in  $kg/kmol$ ) and  $R_{univ} = 8314 J/kmol K$

# Internal Energy and Enthalpy

Internal energy  $e$  ( $[e] = J/kg$ )

Enthalpy  $h$  ( $[h] = J/kg$ )

$$h = e + p\nu = e + \frac{p}{\rho} \text{ (valid for all gases)}$$

For any gas in thermodynamic equilibrium,  $e$  and  $h$  are functions of only two thermodynamic variables (*any two variables may be selected*) e.g.

$$e = e(T, \rho) \text{ or } h = h(T, p)$$

# Internal Energy and Enthalpy

Special cases:

Thermally perfect gas:

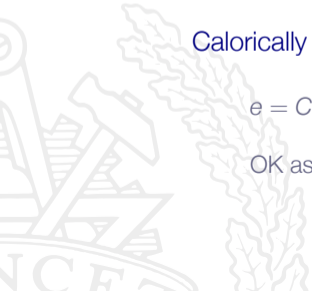
$$e = e(T) \text{ and } h = h(T)$$

OK assumption for air at near atmospheric conditions and  $100K < T < 2500K$

Calorically perfect gas:

$$e = C_v T \text{ and } h = C_p T \text{ (} C_v \text{ and } C_p \text{ are constants)}$$

OK assumption for air at near atmospheric pressure and  $100K < T < 1000K$



# Specific Heat

For thermally perfect (and calorically perfect) gas

$$C_p = \left( \frac{\partial h}{\partial T} \right)_p, \quad C_v = \left( \frac{\partial e}{\partial T} \right)_v$$

since  $h = e + p/\rho = e + RT$  we obtain:

$$C_p = C_v + R$$

The ratio of specific heats,  $\gamma$ , is defined as:

$$\gamma \equiv \frac{C_p}{C_v}$$



# Specific Heat

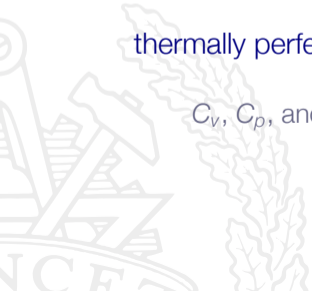
Important!

calorically perfect gas:

$C_v$ ,  $C_p$ , and  $\gamma$  are constants

thermally perfect gas:

$C_v$ ,  $C_p$ , and  $\gamma$  will depend on temperature



# Specific Heat

$$C_p - C_v = R$$

$$C_p - C_v = R$$





# Specific Heat

$$C_p - C_v = R$$

divide by  $C_v$

$$C_p - C_v = R$$

divide by  $C_p$



# Specific Heat

$$C_p - C_v = R$$

divide by  $C_v$

$$\gamma - 1 = \frac{R}{C_v}$$

$$C_p - C_v = R$$

divide by  $C_p$

$$1 - \frac{1}{\gamma} = \frac{\gamma - 1}{\gamma} = \frac{R}{C_p}$$



# Specific Heat

$$C_p - C_v = R$$

divide by  $C_v$

$$\gamma - 1 = \frac{R}{C_v}$$

$$C_v = \frac{R}{\gamma - 1}$$

$$C_p - C_v = R$$

divide by  $C_p$

$$1 - \frac{1}{\gamma} = \frac{\gamma - 1}{\gamma} = \frac{R}{C_p}$$

$$C_p = \frac{\gamma R}{\gamma - 1}$$

# Specific Heat

$$C_p - C_v = R$$

divide by  $C_v$

$$\gamma - 1 = \frac{R}{C_v}$$

$$C_v = \frac{R}{\gamma - 1}$$

$$C_p - C_v = R$$

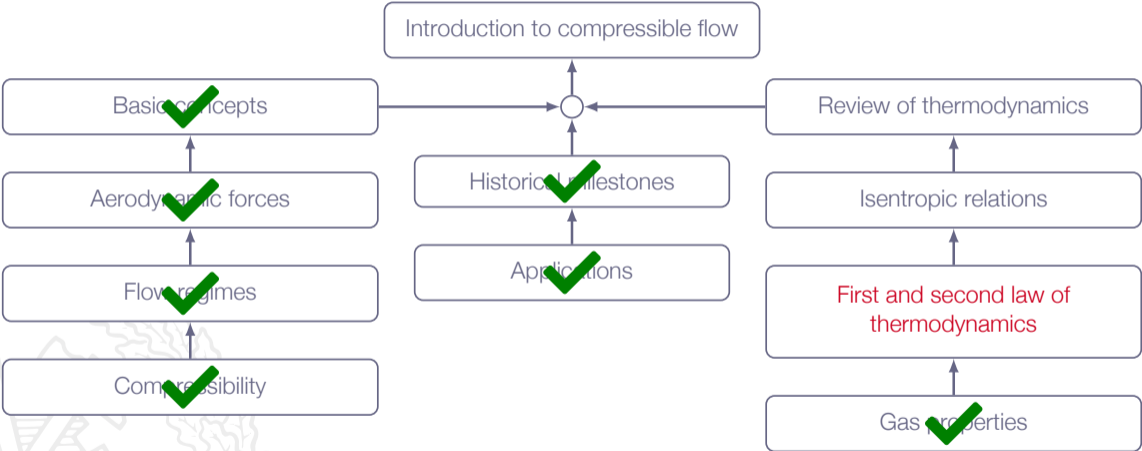
divide by  $C_p$

$$1 - \frac{1}{\gamma} = \frac{\gamma - 1}{\gamma} = \frac{R}{C_p}$$

$$C_p = \frac{\gamma R}{\gamma - 1}$$

valid for both thermally perfect and calorically perfect gas!

# Roadmap - Introduction to Compressible Flow



# First Law of Thermodynamics

A fixed mass of gas, separated from its surroundings by an imaginary flexible boundary, is defined as a **system**. This system obeys the relation

$$de = \delta q - \delta w$$

where

$de$  is a change in internal energy of system

$\delta q$  is heat added to the system

$\delta w$  is work done by the system (on its surroundings)

**Note!**  $de$  only depends on starting point and end point of the process while  $\delta q$  and  $\delta w$  depend on the actual process also

# First Law of Thermodynamics

Examples:

Adiabatic process:

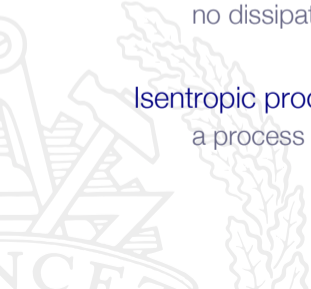
$$\delta q = 0.$$

Reversible process:

no dissipative phenomena (*no flow losses*)

Isentropic process:

a process which is both adiabatic and reversible



# First Law of Thermodynamics

Reversible process:

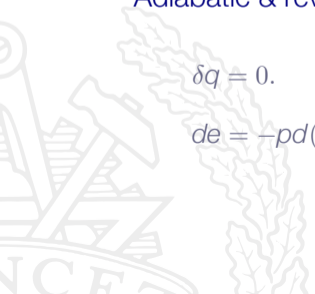
$$\delta w = p d\nu = p d(1/\rho)$$

$$de = \delta q - p d(1/\rho)$$

Adiabatic & reversible process:

$$\delta q = 0.$$

$$de = -p d(1/\rho)$$





# Entropy

Entropy  $s$  is a property of all gases, uniquely defined by any two thermodynamic variables, e.g.

$$s = s(p, T) \text{ or } s = s(\rho, T) \text{ or } s = s(\rho, p) \text{ or } s = s(e, h) \text{ or } \dots$$



# Second Law of Thermodynamics

Concept of entropy  $s$ :

$$ds = \frac{\delta q_{rev}}{T} = \frac{\delta q}{T} + ds_{ir} \text{ where } ds_{ir} > 0. \text{ and thus}$$

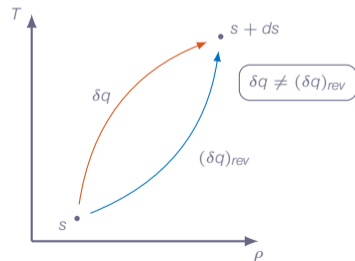
$$ds \geq \frac{\delta q}{T}$$

# Second Law of Thermodynamics

Concept of entropy  $s$ :

$$ds = \frac{\delta q_{rev}}{T} = \frac{\delta q}{T} + ds_{ir} \text{ where } ds_{ir} > 0. \text{ and thus}$$

$$ds \geq \frac{\delta q}{T}$$



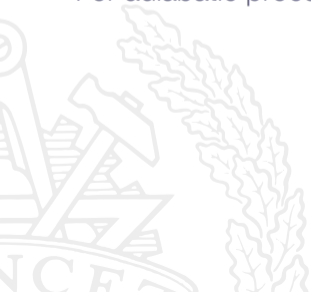
# Second Law of Thermodynamics

In general:

$$ds \geq \frac{\delta q}{T}$$

For adiabatic processes:

$$ds \geq 0.$$



# Calculation of Entropy

For reversible processes ( $\delta w = pd(1/\rho)$  and  $\delta q = Tds$ ):

$$de = Tds - pd \left( \frac{1}{\rho} \right) \Leftrightarrow Tds = de + pd \left( \frac{1}{\rho} \right)$$

from before we have  $h = e + p/\rho \Rightarrow$

$$dh = de + pd \left( \frac{1}{\rho} \right) + \left( \frac{1}{\rho} \right) dp \Leftrightarrow de = dh - pd \left( \frac{1}{\rho} \right) - \left( \frac{1}{\rho} \right) dp$$

# Calculation of Entropy

For thermally perfect gases,  $p = \rho RT$  and  $dh = C_p dT \Rightarrow ds = C_p \frac{dT}{T} - R \frac{dp}{p}$

Integration from starting point (1) to end point (2) gives:

$$s_2 - s_1 = \int_1^2 C_p \frac{dT}{T} - R \ln \left( \frac{p_2}{p_1} \right)$$

and for calorically perfect gases

$$s_2 - s_1 = C_p \ln \left( \frac{T_2}{T_1} \right) - R \ln \left( \frac{p_2}{p_1} \right)$$

# Calculation of Entropy

If we instead use  $de = C_v dT$  we get

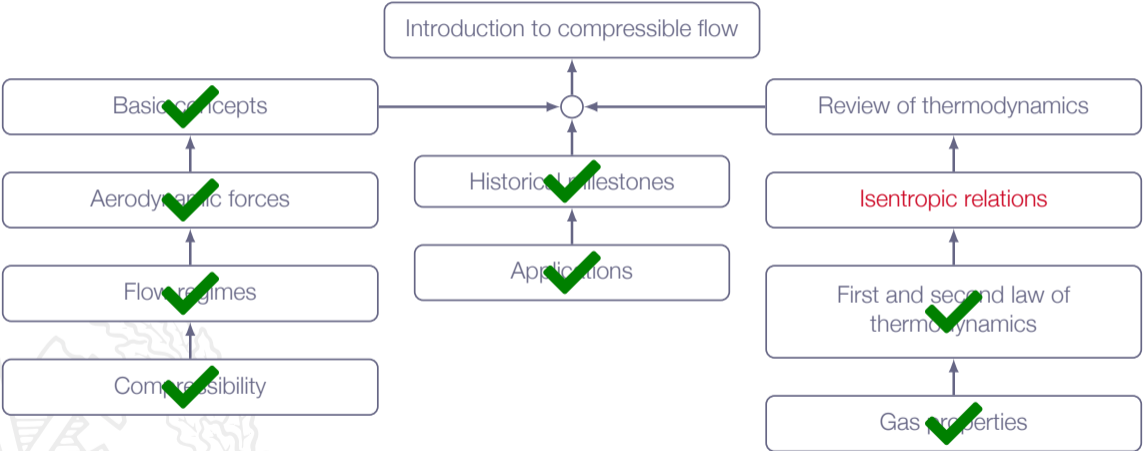
for thermally perfect gases

$$s_2 - s_1 = \int_1^2 C_v \frac{dT}{T} - R \ln \left( \frac{\rho_2}{\rho_1} \right)$$

and for calorically perfect gases

$$s_2 - s_1 = C_v \ln \left( \frac{T_2}{T_1} \right) - R \ln \left( \frac{\rho_2}{\rho_1} \right)$$

# Roadmap - Introduction to Compressible Flow





# Isentropic Relations

For calorically perfect gases, we have

$$s_2 - s_1 = C_p \ln \left( \frac{T_2}{T_1} \right) - R \ln \left( \frac{\rho_2}{\rho_1} \right)$$

For adiabatic reversible processes:

$$ds = 0. \Rightarrow s_1 = s_2 \Rightarrow C_p \ln \left( \frac{T_2}{T_1} \right) - R \ln \left( \frac{\rho_2}{\rho_1} \right) = 0 \Rightarrow$$

$$\ln \left( \frac{\rho_2}{\rho_1} \right) = \frac{C_p}{R} \ln \left( \frac{T_2}{T_1} \right)$$

# Isentropic Relations

$$\text{with } \frac{C_p}{R} = \frac{C_p}{C_p - C_v} = \frac{\gamma}{\gamma - 1} \Rightarrow$$

$$\frac{p_2}{p_1} = \left( \frac{T_2}{T_1} \right)^{\frac{\gamma}{\gamma - 1}}$$



# Isentropic Relations

Alternatively, using  $s_2 - s_1 = 0 = C_v \ln \left( \frac{T_2}{T_1} \right) - R \ln \left( \frac{\rho_2}{\rho_1} \right) \Rightarrow$

$$\frac{\rho_2}{\rho_1} = \left( \frac{T_2}{T_1} \right)^{\frac{1}{\gamma-1}}$$



# Isentropic Relations - Summary

For an isentropic process and a calorically perfect gas we have

$$\frac{p_2}{p_1} = \left(\frac{\rho_2}{\rho_1}\right)^\gamma = \left(\frac{T_2}{T_1}\right)^{\frac{\gamma}{\gamma-1}}$$

A.K.A. the **isentropic relations**



# Roadmap - Introduction to Compressible Flow

